INTRODUCTION

When a piece of technical equipment is marketed successfully for over 65 years, it is inevitable that a large body of experience will develop from the use of that equipment. Procedures are established, papers are published, standards are accepted, and a vast informal grapevine of advice grows amidst the community of users. Such is the case with the Brookfield Viscometer. Accepted as a standard of viscosity measurement around the world, the Brookfield Viscometer is the nucleus of a library of information that encompasses the experiences of thousands of users in a seemingly endless variety of applications.

This library, however, is not gathered conveniently together in any single location. It is fragmented, scattered here and there in technical journals, in test reports, in the notes made by technicians, researchers, and quality control people. For many users (particularly those new to the field of viscosity measurement), it is extremely difficult to gain access to information generated outside their own company or industry. Brookfield Engineering Laboratories has for many years acted as a clearinghouse for this type information, reprinting a variety of technical papers on the subject of viscosity measurement and making them available at no cost. This program has helped many people benefit from the experiences of others.

There is a middle ground, however, between the specific technical information provided in these papers and the basic operating procedures outlined in an instruction manual for your instrument. We have been requested many times over the years to publish a book that would bridge the gap between the elementary and the advanced, a sort of extended "user's manual" that would guide the way for the person wishing to explore in greater depth the field of viscosity measurement, with an emphasis on Brookfield equipment.

The book you hold in your hand is the result of those requests. It does not replace your instruction manual, nor does it replace the specific technical papers already or yet to be published. It is also not a textbook on rheology. Rather, it is a guide to help point out the way to getting more from your Brookfield Viscometer. It does this in several ways:

- by offering practical advice on the use and maintenance of the Brookfield Viscometer based on our experience and that of our customers;
- by suggesting ways in which specific pieces of hardware may be used to solve viscosity measurement problems;
- by explaining the basic principles of rheology and their relation to measurements made with Brookfield equipment;
- by discussing factors that affect rheological behavior and how these may be controlled;
- by outlining advanced mathematical procedures for detailed analysis of viscosity data;
- by consolidating a variety of useful range tables, formulas, and specifications for many Brookfield Viscometers and accessories.

We hope that you will find this book useful and refer to it often. It is our attempt to answer all at once many of the questions we have been asked over the years. If you have any questions that are not answered here, or if you want to suggest improvements or changes for future editions, please feel free to contact us. It was, after all, the input of people like yourself that made this book possible in the first place.

CHAPTER 1

1.1 Why Make Rheological Measurements?

Anyone beginning the process of learning to think Rheo-Logically must first ask the question, "Why should I make a viscosity measurement?" The answer lies in the experiences of thousands of people who have made such measurements, showing that much useful behavioral and predictive information for various products can be obtained, as well as knowledge of the effects of processing, formulation changes, aging phenomena, etc.

A frequent reason for the measurement of rheological properties can be found in the area of quality control, where raw materials must be consistent from batch to batch. For this purpose, flow behavior is an indirect measure of product consistency and quality.

Another reason for making flow behavior studies is that a direct assessment of processability can be obtained. For example, a high viscosity liquid requires more power to pump than a low viscosity one. Knowing its rheological behavior, therefore, is useful when designing pumping and piping systems.

It has been suggested that rheology is the most sensitive method for material characterization because flow behavior is responsive to properties such as molecular weight and molecular weight distribution. This relationship is useful in polymer synthesis, for example, because it allows relative differences to be seen without making molecular weight measurements. Rheological measurements are also useful in following the course of a chemical reaction. Such measurements can be employed as a quality check during production or to monitor and/or control a process. Rheological measurements allow the study of chemical, mechanical, and thermal treatments, the effects of additives, or the course of a curing reaction. They are also a way to predict and control a host of product properties, end use performance and material behavior.

1.2 Thinking Rheo-Logically

To begin, consider the question, "Can some rheological parameter be employed to correlate with an aspect of the product or process?" To determine this, an instinct must be developed for the kinds of chemical and physical phenomena which affect the rheological response. For the moment, assume this information is known and several possibilities have been identified. The next step is to gather preliminary rheological data to determine what type of flow behavior is characteristic of the system under consideration. At the most basic level, this involves making measurements with whichever Brookfield Viscometer is available and drawing some conclusions based on the descriptions of flow behavior types in Chapter 4.

Once the type of flow behavior has been identified, more can be understood about the way components of the system interact (more information on what affects the rheological property can be found in Section 4.7). The data thus obtained may then be fitted to one of the mathematical models which have been successfully used with Brookfield instruments. Many of these models may be found in Chapter 5.

Such mathematical models range from the very simple to the very complex. Some of them merely involve the plotting of data on graph paper; others require calculating the ratio of two numbers. Some are quite sophisticated and require use of programmable calculators or computers. This kind of analysis is the best way for getting the most from our data and often results in one of two "constants" which summarize the data and can be related to product or process performance.

Once a correlation has been developed between rheological data and product behavior, the procedure can then be reversed and rheological data may be used to predict performance and behavior.

1.3 Three Schools of Thought on Viscosity Measurement

In our experience there are basically three schools of thought on the use of viscometers in applications rheology. We present them here and invite you to decide which you fall into, remembering that there is no "right" one and that each has its merits.

1.3.1 The Pragmatic School

The first school of thought is the most pragmatic. The person who adheres to this school cares only that the Brookfield Viscometer generates numbers that tell something useful about a product or process. This person has little or no concern about rheological theory and measurement parameters expressed in absolute terms. Quality control and plant production applications are typical of this category.

1.3.2 The Theoretical School

The second school of thought involves a more theoretical approach. Those adhering to this school know that some types of Brookfield Viscometers will not directly yield defined shear rates and absolute viscosities for non-Newtonian fluids. However, these people often find that they can develop correlations of "dial viscosity" with important product or process parameters. Many people follow this school of thought. The applications rheology literature is replete with statements along the line of "I know the data isn't academically defined, but I keep this fact in mind and treat the multi-point rheology information as if it were." In many cases, this produces eminently satisfying results and eliminates the necessity of buying a highly sophisticated and very expensive piece of rheological equipment.

1.3.3 The Academic School

The third school of thought is quite academic in nature. People adhering to this school require that all measurement parameters, particularly shear rate and shear stress, be defined and known. They need equipment with defined geometries such as cone and plate or coaxial cylinders. Examples from the Brookfield line would be the Wells-Brookfield Cone/Plate and CAP Viscometers and the UL adapter, Small Sample Adapter, Thermosel, Din Adapter and Spiral Adapter accessories, as well as the PVS Rheometer. With this equipment the shear rate is defined and accurate absolute viscosities are obtained directly.

That, then, is our view of the three schools of thought on viscosity measurement. You may need to think in terms of any or all of these depending on your background, approach, goals, and type of equipment available. Brookfield Viscometer users fall into all three; the following chapters present information of use to each.

CHAPTER 2

2.1 Equipment for Specific Situations

The purpose of this chapter is to provide an overview of Brookfield's entire line of Viscometers and related accessories, and to suggest ways in which these products may be helpful in solving specific viscosity measurement problems. This information will be useful to people adhering to all three schools of thought on viscosity measurement.

The equipment has been organized into functional groups to help you quickly zero in on the items of most interest to you:

- 2.1.1 Viscometers
- 2.1.2 Spindle Geometries
- 2.1.3 Temperature Control
- 2.1.4 Small Sample Volume
- 2.1.5 Low Viscosity
- 2.1.6 High Temperature
- 2.1.7 Defined Shear Rate
- 2.1.8 High Shear Rate
- 2.1.9 Non-Flowing Sample Materials
- 2.1.10 Fumes and Hazardous Locations
- 2.1.11 Process Control

2.1.1 Viscometers

Brookfield laboratory Viscometers are available in three basic types: dial-reading (analog), digital, and programmable. The most significant difference between them is the manner in which the viscosity reading is displayed. The dial-reading type is read by noting the position of a pointer in relation to a rotating dial; the Digital type is read by means of a 3-digit LED display. In addition, the Digital Viscometer includes a 0-10mv output that may be connected to a variety of devices, such as remote displays, controllers, and recorders.

In most respects dial-reading and Digital Viscometers are functionally similar. The operating procedures for both are essentially the same, they are available in the same model variations, they accept the same Brookfield accessories, and are generally interchangeable (model for model) in most viscosity specifications requiring Brookfield Viscometers.

The dial-reading type is the least expensive Brookfield Viscometer and is suitable for most applications where samples are to be tested over a short period of time and a permanent detailed record of rheological behavior is not required. This is due to the fact that while the Viscometer rotates continuously, readings may be made only intermittently, when the pointer passes under the vision glass, or when the reading is held and the Viscometer stopped. Long term viscosity tests necessitate frequent operator attention, and some fast-acting processes dictate continuous monitoring.

The Digital Viscometer, with its continuous sensing and recorder output, is more suited to such situations. It may be left unattended for long periods, and the recorder speed may be adjusted to provide a detailed record of even the fastest rheological processes. In addition, many operators prefer a digital display, which eliminates the interpolation sometimes necessary when reading a dial. The Digital Viscometer, however, cannot be hand-held during use, unlike the dial-reading type. Both types offer equivalent accuracy.

All Brookfield laboratory Viscometers are available both in standard spindle and cone/plate configurations. See Section 2.1.8 for more information on cone/plate spindle geometry.

It is not possible to convert a dial-reading Viscometer to a Digital Viscometer, or to connect a recorder, printer or PC to it.

There are many variations of the standard Viscometer models available, such as intermediate spring torques, alternative rotational speeds, and various physical modifications. Please consult Brookfield Engineering Laboratories or your dealer for details and availability.

2.1.2 Spindle Geometries

All Brookfield Viscometers are supplied with spindles suitable for most applications within the viscosity range of the instrument. There are, however, situations where specialized spindle geom-

etries are necessary to obtain optimum results. Brookfield has available a wide variety of spindles and accessories to fulfill this need. Many are listed in this section.

All Brookfield Viscometer spindles are constructed of 300 series stainless steel for maintenance-free service in most applications; some are available coated for maximum corrosion resistance. Please inquire about special spindle materials and configurations for unusual applications.

Disc Spindles

Provided as standard equipment with LV (spindles #2 and #3) and RV/HA/HB models (spindles #1 through #6), these are general-purpose spindles for use in containers of 600 mL capacity or larger. Disc spindles produce accurate, reproducible apparent viscosity determinations in most fluids. The results obtained can be converted into viscosity functions by a mathematical procedure outlined in Technical Paper AR-82, available from Brookfield Engineering Laboratories. See Section 2.1.7 for information on spindle geometries that directly provide defined shear rates.

Cylindrical Spindles

These spindles (LV #1 and #4, RV/HA/HB #7) provide a defined spindle geometry for calculating shear stress and shear rate values as well as viscosity. In all other respects their operating parameters are similar to those of disc spindles. Because their defined geometry facilitates mathematical analysis, cylindrical spindles are particularly valuable when measuring non-Newtonian fluids. They are applicable to any Brookfield Viscometer model with the use of the appropriate range sheet. Cylindrical equivalents of the LV #2 and #3 disc spindles are also available. See Section 2.1.7 for information on other defined shear rate geometries.

Coaxial Cylinders

Coaxial-cylinder geometry is indicated for applications where extremely well-defined shear rate and shear stress data is required, particularly when the sample volume is relatively small. Several Brookfield accessories feature coaxial-cylinder geometry; each also has unique advantages for specific situations. These accessories are: the Small Sample Adapter (Section 2.1.4), the UL Adapter (Section 2.1.5), the Thermosel (Section 2.1.6), and the DIN Adapter (Section 2.1.4).

Cone/Plate Geometry

Cone/plate geometry offers absolute viscosity determinations with precise shear rate and shear stress information readily available. The sample volumes required are extremely small and the sample cup is jacketed for temperature control. Cone/plate geometry is particularly suitable for advanced rheological analysis of non-Newtonian fluids. It is available on the Wells-Brookfield Cone/Plate Viscometer (see Section 2.1.8 for more information).

T-Bar Spindles

Generally used in conjunction with the Helipath Stand accessory (with which they are supplied as standard equipment), T-bar spindles make possible the measurement of non-flowing or slow-flowing materials such as pastes, gels, and creams. See Section 2.1.9.

2.1.3 Temperature Control

In order to ensure maximum accuracy and reproducibility in many viscosity measurement procedures, temperature control is highly recommended. The following systems are available from Brookfield:

Temperature Baths

Constant-temperature baths are suitable for most viscosity measurement applications. They are available in two basic types: circulating, for use with jacketed devices such as the Wells-Brookfield Cone/Plate Viscometer (Section 2.1.8) and the Small Sample Adapter (Section 2.1.5); and reservoir/circulating, for all applications (this type can be used with jacketed devices as well as with any sample container that can be immersed in the bath's reservoir). Temperature baths are generally limited to a maximum operating temperature of approximately 120°C (depending on the bath fluid used), and usually require auxiliary cooling devices for operation at or below ambient temperature. Refrigerated baths are also available. Contact Brookfield Engineering Laboratories or your dealer for more information.

Thermosel System

This system is designed for the measurement of small samples in the temperature range of approximately 40 to 300°C. Unlike a temperature bath, the Thermosel doesn't utilize a fluid medium for temperature control. For more information, see Section 2.1.6.

2.1.4 Small Sample Volume

The standard sample container for most Brookfield Viscometers is a 600 mL low form Griffin beaker. Users often find it desirable or necessary to measure samples of smaller volume. Several Brookfield products feature small sample volumes.

Small Sample Adapter

Specifically designed to facilitate the measurement of small samples, the Small Sample Adapter is a jacketed, coaxial-cylinder accessory that is compatible with all Brookfield Viscometers with the exception of cone/plate types. Depending on the model selected, the Small Sample Adapter utilizes sample volumes of 2.0 to 16.0 mL. Also depending on model, the Small Sample Adapter will measure viscosities from 5 cP to 10,000,000 cP at shear rates from 0.066 to 93.0 reciprocal seconds. The Small Sample Adapter's jacketed design permits

connection to a circulating-type bath for excellent temperature control up to a recommended maximum of 100° C.

UL Adapter

The UL Adapter is primarily intended to allow viscosity measurements in ranges below those normally measurable by a particular Viscometer. When used with its removable end cap in place, the UL Adapter measures a sample volume of 16.0 mL. For more information, see Section 2.1.5.

DIN Adapter

The DIN Adapter, like the UL Adapter, is designed to measure in ranges below those normally measured with a particular Viscometer. The DIN Adapter utilizes additional DIN spindles for measurement ranges from 1 cP to 50,000 cP and conforms to DIN 53019.

Thermosel System

The Thermosel System allows the measurement of viscosity at temperatures to 300°C. It incorporates coaxial-cylinder spindle geometry that uses a sample volume of 8.0 to 13.0 mL, depending on the spindle utilized. See Section 2.1.6.

Wells-Brookfield Cone/Plate & CAP Viscometers

When sample volume is extremely limited, it may be necessary to use the Wells-Brookfield Cone/Plate Viscometer. It requires a sample of only 0.5 to 2.0 mL, depending on spindle. More data on this instrument will be found in Section 2.1.8.

The CAP Cone/Plate Viscometer requires <1mL for sample volume. See Section 2.1.8 for details.

2.1.5 Low Viscosity

Each Brookfield Viscometer measures a wide range of viscosities; however, it occasionally becomes necessary to measure viscosities below the normal range of the instrument. Several pieces of Brookfield equipment offer this capability:

UL Adapter

This accessory was specifically designed to provide greater sensitivity at low viscosities for the LV series Viscometers; it can, however, be used on any model Brookfield Viscometer except cone/plate types. When mounted on an LVF or LVT Viscometer, the UL Adapter provides a viscosity range of 1.0 to 10.0 cP and a defined shear rate of 73.4 reciprocal seconds at 60 RPM. For other Viscometer models, the minimum measurable viscosity with the UL Adapter in place is: RVT, 6.4 cP; HAT, 12.8 cP; HBT, 51.2 cP. The UL Adapter features coaxial-cylinder geometry with a removable polyethylene end cap for the outer cylinder. With the end cap in place, the Adapter holds a sample volume of 16.0 mL and can be immersed in a bath for temperature control up to a recommended maximum of 100°C; with the cap removed it may be used in sample containers of almost any size.

Small Sample Adapter

With some spindle/chamber combinations, the Small Sample Adapter permits measurement of viscosities below the Viscometer's normal range. Check the applicable range sheet for details. More information on the Small Sample Adapter can be found in Section 2.1.4.

Thermosel System

With certain spindles, the Thermosel System provides increased sensitivity at low viscosities; check the applicable range sheet for more data. The Thermosel System is discussed in more detail in Section 2.1.6.

Wells-Brookfield Cone/Plate Viscometer

The Wells-Brookfield Cone/Plate Viscometer has low-viscosity capabilities as low as 0.1 cP. See Section 2.1.8 for more information on this instrument.

2.1.6 High Temperature

Measurement of viscosity at high temperature can be simple or complex, depending upon the sample materials and temperature. Sometimes all that is necessary is to increase the distance between the Viscometer and sample material through use of spindle extensions (see Section 2.1.10). In difficult applications, such as the measurement of molten glass, it may be necessary to utilize a specialized furnace and crucible, as well as custom-designed spindles constructed of heat resistance materials (consult with Brookfield Engineering Laboratories for more information on this type application). Between these two extremes, there is Brookfield equipment for most high temperature viscosity measurement applications.

Thermosel System

The Thermosel System is specifically designed for viscosity measurement of small samples in the temperature range of approximately 25 to 300°C. It is usually sold as a complete system including Viscometer, but it is also available as an accessory to your present Viscometer (except cone/plate types).

In addition to the Viscometer, the Thermosel System consists of a special coaxial-cylinder spindle and sample chamber, an electric heating apparatus called a thermocontainer, and a digital proportional temperature controller with RTD sensor. The Thermosel System is available in three variations: System 1 is a manual unit with a dial-reading Viscometer; System 2 includes a Digital Viscometer and outputs for recording viscosity and temperature; and System 3, which adds the capabilities of a fully programmable temperature controller to the features of System 2.

The Thermosel System requires small sample volumes (8.0 to 13.0 mL, depending on spindle), and its coaxial-cylinder spindle geometry provides defined shear rates in the range of 0.08 to 93.0 reciprocal seconds, depending on spindle and Viscometer model.

Temperature Baths

Brookfield Temperature Baths are also suitable for viscosity measurements at high temperature. They generally are limited to a maximum operating temperature of 120°C. For more information, see Section 2.1.2.

2.1.7 Defined Shear Rate

For applications where viscosity data must be expressed in absolute terms, it is necessary to use a spindle geometry for which shear rate and shear stress values can be calculated. Such defined operating parameters are found in the following Brookfield instruments and accessories. Consult the referenced sections for more information about these products:

Cylindrical Spindles	2.1.2
UL Adapter	2.1.5
DIN Adapter	2.1.4
Small Sample Adapter	2.1.4
Thermosel System	2.1.6
Wells-Brookfield Cone/Plate Viscometer	2.1.8
CAP Viscometer	2.1.8

2.1.8 High Shear Rate

Brookfield Viscometers are, by design, relatively low-shear instruments. The maximum shear rate achievable with most spindle configurations is usually less than 100 reciprocal seconds. Defined shear rates in the range of up to 300 reciprocal seconds can be generated by some Viscometer models when used in conjunction with the UL Adapter (Section 2.1.5), the Small Sample Adapter (Section 2.1.4), or as part of the Thermosel System (Section 2.1.6). For shear rates in excess of 300 reciprocal seconds it is usually necessary to use the Wells-Brookfield Cone/Plate Viscometer, CAP Viscometer or PVS Rheometer.

Wells-Brookfield Cone/Plate Viscometer

The Wells-Brookfield Cone/Plate Viscometer will determine the absolute viscosity of small samples under conditions of defined shear rate and shear stress. Its cone and plate spindle geometry requires a sample volume of only 0.5 to 2.0 mL and generates shear rates in the range of 0.6 to l500 reciprocal seconds (depending on Viscometer model and spindle used). The instrument's sample cup is jacketed for excellent temperature control.

Depending on the particular Viscometer model and spindle in use, the Wells-Brookfield Cone/Plate Viscometer will measure viscosities from 0.5 to 1.5 million cP (although no single instrument will cover this range, the use of several spindles will allow one Viscometer to measure a wide range of viscosities).

The Wells-Brookfield Cone/Plate Viscometer is available in dial-reading and Digital versions. A temperature bath is optional and highly recommended for precise and reproducible viscosity measurements.

The cone and plate spindle geometry is available only on the Wells-Brookfield Cone/Plate Viscometer; it is not available as an accessory or modification of other Brookfield Viscometers. It is possible to use this Viscometer with standard disc and cylindrical spindles, however; an extension for the laboratory stand is required to provide sufficient clearance under the Viscometer.

CAP Viscometer

The Brookfield CAP series of Cone/Plate Viscometers offer high shear rates and variable speeds in an instrument optimized for R&D and QC applications such as paints, coatings, resins, inks, cosmetics, pharmaceuticals and foods. These series of viscometers offer high shear rate with integrated temperature control for test sample volume of less than 1 mL.

The CAP series operates with automatic cone gap positioning and viscosity range calibration and is offered as two models: CAP 1000 and CAP 2000. The CAP 1000 is a single speed viscometer and has a fixed shear rate at 750 RPM on 50 Hz and 9000 RPM on 60 Hz and generates shear rates at 12,000 or 3,000 sec^{-1} at 60 Hz and 10,000 or 2,500 sec^{-1} at 50 Hz. Viscosity ranges from .25 to 100 Poise (0.25 to 10 Pa•s) depending on the cone spindle used. The CAP 2000 is a variable-speed instrument and has variable shear rate capability over the speed range from 50 to 2,000 RPM. This instrument generates shear rates from 166 to 26, 600 sec^{-1} at viscosity ranges from 0.1 to 1,500 Poise (0.1 to 150 Pa•s). Both the CAP 1000 and CAP 2000 are accurate to ±2% of the full scale range and meet industry test standards BS3900, ISO 2884, and ASTM D-4287.

PVS Rheometer

The Brookfield PVS Rheometer is a portable unit designed for measuring viscosity at high pressure and temperature. It's ability to measure viscosity over a pressure range from abient up to 1,000 psi and a temperature range of -40°C to 200°C makes it ideal for applications such as oil and gas well drilling fluids, pulp and paper, plastics, petrochemicals, and aerosol based products.

The PVS Rheometer operates at shear rates from 0.01 sec^{-1} to 1,700 sec^{-1} corresponding to speed ranges from 0.05 to 1,000 RPM . The PVS Rheometer torque sensor is unaffected by changes in pressure or temperature; the placement of barings outside the pressurized sample volume virtually elminates the need for maintenance.

2.1.9 Non-Flowing Sample Materials

Non-flowing or slow-flowing sample materials such as pastes, creams, and gels present special problems in viscosity measurement. Conventional rotating spindles tend to "channel" (push the sample material aside), resulting in a continuously decreasing Viscometer reading that is of little value. The Helipath Stand is an accessory that eliminates

this problem.

Helipath Stand

The Helipath Stand is a motorized stand to which any Brookfield Viscometer can be attached. The Stand slowly raises and lowers the Viscometer (at a rate of 7/8-inch per minute) while a special T-bar spindle rotates in the sample material. The crossbar of the spindle thus continuously cuts into fresh material, describing a helical path through the sample as it rotates. The "channeling" effect of conventional spindles is completely eliminated permitting meaningful viscosity/consistency measurements to be made. A set of six T-bar spindles and a special coupling are included with the Helipath Stand.

Spiral Adapter

The Brookfield Spiral Adapter accessory is a pump-type sensor that directly measures viscosity of pastes, including applications such as solder paste, foods, cosmetics and pharmaceuticals. The Spiral Adapter has an inner, threaded spindle surrounded by a concentric outer cylinder. This combination causes the sample to be continually pumped up through the Spiral Adapter. The material reaches a steady state of flow during which viscosity is measured. The steady-state measurement is less sensitive to sample handling and minor material variations than other viscosity measuring methods.

2.1.10 Special Accessory Items

The following items can be purchased for use with Brookfield Viscometers/Rheometers.

Quick Connect

The Brookfield Quick Connect accessory is designed to quickly attach or remove a spindle from a Brookfield Viscometer/Rheometer resulting in time savings and elimination of cross threading. The Quick Connect accessory is made of stainless steel and is used with LV, RV/HA/HA disk spindles as well as T-bar couplings.

Spindle Extensions

Spindle extensions are suitable for applications utilizing standard disc or cylindrical spindles where distance between the Viscometer and the sample materia must be increased (up to 6 feet maximum). Type D extensions are installed between the Viscometer and the spindle, and are suitable for applications where depth of the spindle immersion can be observed. Type S extensions include the immersed portion of the spindle and are used where depth of immersion is not observable.

Purge Fittings

A purge fitting may be provided on the pivot housing of any Viscometer. An inert gas such as nitrogen is introduced under low pressure through the purge fitting, creating a positive pressure inside the Viscometer housing which prevents entry of fumes and vapors.

Purge fittings are also available for sample cups of the Wells-Brookfield Cone/Plate Viscometer and the Thermosel System to provide a controlled atmosphere for the sample being tested.

Mercury Switch (Dial Viscometer Only)

In situations where potentially explosive or flammable fumes are present, precautions must be taken to eliminate any sources of sparking within the Viscometer. Since all Brookfield Viscometers utilize a brushless motor, the only potential source of sparking within the Viscometer is the power switch. Replacement of the standard switch with a non-sparking mercury switch is an inexpensive way of making the Viscometer "explosion-safe" and is adequate for applications where danger of explosion is relatively slight, but additional safety is desired. Be aware, however, of other possible sources of sparking outside the Viscometer, such as the line cord plug, and take appropriate precautions. The mercury switch is available for dial-reading Viscometers only.

Explosion-Proof Construction (Dial Viscometer Only)

When the danger of explosion is great due to the presence of flammable fumes or other factors, use of approved explosion-proof equipment may be required. Brookfield dial-reading Viscometers (except cone/plate types) are available in Underwriters' Laboratory (UL) approved explosion-proof versions. These instruments are approved for Class I, Group D hazardous locations. The Digital Viscometers and Rheometers are not available with explosion-proof construction.

Electrically operated Brookfield accessories, such as the Helipath Stand and the Thermosel, are not available in explosion-proof versions. They can be used with explosion-proof Viscometers (sometimes requiring special adapters), but only in non-hazardous environments.

2.1.11 Fumes and Hazardous Locations

Whenever fumes and vapors are present that could enter the Viscometer, care should be taken to prevent such entry. When the fumes are explosive or flammable, special precautions are required not only for protection of the Viscometer, but for the safety of nearby personnel. The preceding sections give an overview of accessories and modifications available for such applications.

2.1.12 Process Control

Practical application of viscosity data obtained in the laboratory often involves use of on-line process viscometers and viscosity controllers. Brookfield manufactures a complete line of instrumentation that has been applied to a wide variety of process control applications. Please contact Brookfield Engineering Laboratories for more information.

CHAPTER 3

3.1 Why You Should Read This Chapter

The purpose of this chapter is to provide the Viscometer user with information necessary to make meaningful viscosity measurements. It will describe the mechanical components of the Brookfield Viscometer and suggest some useful operational techniques.

Those adhering strictly to the Pragmatic school of viscosity measurement may not wish to read any further than this chapter. All users, however, should read it before moving on; a good grounding in basic Viscometer operation will facilitate advancement to more sophisticated techniques.

3.2 How the Brookfield Viscometer Works

The Brookfield Viscometer is of the rotational variety. It measures the torque required to rotate an immersed element (the spindle) in a fluid. The spindle is driven by a motor through a calibrated spring; deflection of the
spring is indicated by a pointer and dial (or a digital display). By utilizing a multiple speed transmission and interchangeable spindles, a variety of viscosity ranges can be measured, thus enhancing versatility of the instrument.

For a given viscosity, the viscous drag, or resistance to flow (indicated by the degree to which the spring winds up), is proportional to the spindle's speed of rotation and is related to the spindle's size and shape (geometry). The drag will increase as the spindle size and/or rotational speed increase. It follows that for a given spindle geometry and speed, an increase in viscosity will be indicated by an increase in deflection of the spring. For any Viscometer model, the minimum range is obtained by using the largest spindle at the highest speed; the maximum range by using the smallest spindle at the slowest speed. Measurements made using the same spindle at different speeds are used to detect and evaluate rheological properties of the test fluid. These properties and techniques are discussed in Chapters 4 and 5.

The Viscometer is composed of several mechanical subassemblies. See Figures 3-1 for a schematic view of the major components of a basic dial-reading Viscometer.

The drive motor and multiple-speed transmission are located at the top of the instrument inside the housing to which the nameplate is attached. The Viscometer main case contains a calibrated beryllium-copper spring, one end of which is attached to the pivot shaft, the other end is connected directly to the dial. This dial is driven by the transmission and in turn drives the pivot shaft through the calibrated spring. In dial-reading models, the pointer is connected to the pivot shaft and indicates its angular position in relation to the dial. In Digital models, the relative angular position of the pivot shaft is detected by an RVDT (rotary variable displacement transducer) and is read out on a digital display.

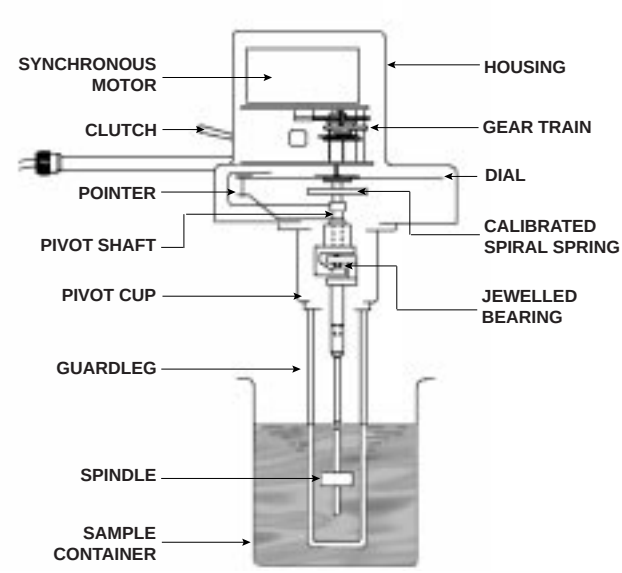


Figure 3-1

Below the main case is the pivot cup through which the lower end of the pivot shaft protrudes. A jewel bearing inside the pivot cup rotates with the dial or transducer; the pivot shaft is supported on this bearing by the pivot point. The lower end of the pivot shaft comprises the spindle coupling to which the Viscometer's spindles are attached.

3.3 Viscosity Measurement Techniques

As with any precision instrument, proper operating techniques will improve effectiveness of the Brookfield Viscometer. A step-by-step procedure for Viscometer operation can be found in the Instruction Manual supplied with each unit, and is not repeated here. Instead, we present recommendations and advice gleaned from over 65 years of customer experience. They form a sound foundation for a viscosity testing procedure and a starting point from which more advanced techniques can be explored.

3.3.1 Record Keeping

We recommend that the following information always be recorded when making a viscosity measurement; viscometer model, spindle (or accessory), rotational speed, container size or dimensions, sample temperature, sample preparation procedure (if any), and whether or not the spindle guardleg was used. Test Report Forms supplied in the instruction manual with each Viscometer are convenient for this purpose.

3.3.2 The Spindle and the Guardleg

Examine each spindle before using it. If it is corroded or damaged to the extent of changing its dimensions, a false viscosity reading may result. Since all spindles are brightly polished when new, any sign of pitting, dulled edges, or other obvious damage should dictate the purchase of a new spindle. If you have an unusual problem along these lines, corrosion-resistant 316 series stainless steel and Teflon-coated spindles are available. Also, special spindle materials can be employed.

When attaching a spindle, remember that it has a **left-hand** thread and must be screwed firmLy to the coupling. Always lift up on the spindle coupling when attaching a spindle to avoid damage to the instrument's pivot point and jewel bearing. After attachment, do not hit the spindle against the side of the sample container since this can damage the shaft alignment. A good procedure to follow is to immerse and position the spindle in the sample fluid before attaching it to the Viscometer.

The spindle guardleg (supplied with some models) protects the spindle from damage and is significant to the Viscometer's calibration when using the #1 or #2 spindle. The guardleg should be used at all times. If it proves necessary or desirable to operate the Viscometer without the guardleg, this fact should be noted when reporting test results. It must be desirable to recalibrate the Viscometer to compensate for the absence of the guardleg. Refer to Section 3.3.10 for this procedure.

Note: spindle guardlegs are provided only on LV and RV models of the dial-reading and Digital Viscometers with standard spindles. HA and HB models, as well as Cone/Plate models, do not require a guardleg. The guardleg is also not used in conjunction with most accessories.

3.3.3 Selecting a Spindle Speed

When performing a test according to an existing specification or procedure, use the spindle and speed specified (after confirming that you have the correct Viscometer model). When conducting an original test, the best method for spindle and speed selection is trial and error. The goal is to obtain a Viscometer dial or display reading between 10 and 100, remembering that accuracy improves as the reading approaches 100 (see Section 3.3.7). If the reading is over 100, select a slower speed and/or a smaller spindle. Conversely, if the reading is under 10, select a higher speed and/or a larger spindle.

If the approximate viscosity of the sample fluid is known, a faster method for honing in on the right spindle/speed combination is available by referring to the Factor Finder supplied with the Viscometer. The goal is to select a combination whose range brackets the estimated viscosity of the sample.

For any given spindle/speed combination, the **maximum** range available is equal to the spindle Factor multiplied by 100. This maximum is also called "Full Scale Range" or "FSR". For Digital Viscometers that have the AUTORANGE key, selecting a speed and spindle and then depressing and holding the AUTORANGE key will cause the screen to display FSR in cP.

The **minimum** recommended range equals the Factor multiplied by 10. For example: a #2 spindle on an LVT Viscometer at 12 RPM has a Factor of 25. The maximum range of this combination is 25 times 100, or 2500 cP. The minimum recommended viscosity that should be measured is 25 times 10, or 250 cP. Therefore, if the viscosity of the sample fluid is estimated to be 4000 cP, another spindle/speed combination must be selected in order to make the measurement. If the sample fluid is around 2000 cP, however, this spindle and speed would be suitable. With a little practice, a quick glance at the Factor Finder will suffice to make an appropriate selection of spindle and speed.

When conducting multiple tests, the same spindle/speed combination should be used for all tests. When a test must be performed at several speeds, select a spindle that produces on-scale readings at all required speeds. This may necessitate using a dial or display reading less than 10, which is acceptable as long as the reduced accuracy of such a reading is recognized.

3.3.4 Sample Container Size

For measurements with standard Viscometer models we recommend a container with an inside diameter of 3 1/4 inches (83 mm) or larger. The usual vessel for this purpose is a 600 mL low form Griffin beaker. Use of a smaller container will result in an increase in viscosity readings, particularly with the #1 and #2 spindle.

When utilizing a smaller container, the simplest approach is to report the dimensions of the container and ignore the probable effect on calibration. As long as the same size container is used for all subsequent tests, there will be no correlation problem.

Alternatively, the Viscometer can recalibrated to compensate for the smaller container as outlined in Section 3.3.10. Also, use of the Small Sample Adapter should be considered. See Section 2.1.4.

3.3.5 Sample Conditions

The sample fluid should be free from entrapped air. Air can be removed by gently tapping the container on a table top or by using a vacuum apparatus.

The sample should be at a constant and uniform temperature. This can be verified by checking the temperature at several different locations within the container. Be sure to bring the sample, spindle, and guardleg to the same temperature before tak-

ing a viscosity reading. Temperature uniformity can often be maintained by agitation prior to a measurement, but first determine that such agitation won't affect viscosity of the sample fluid (see Section 4.7.5). Factors used to calculate viscosity values from the Viscometer readings are independent of temperature.

A constant temperature water bath is used to maintain the desired temperature. Refer to Section 2.1.3 for information on recommended baths.

High temperature work (up to 300°C) may require use of the Thermosel accessory. See Section 2.1.6.

Homogeneity of the sample is also quite important, especially in dispersed systems where settling can occur. In many cases, simple stirring just prior to the test will keep the components dispersed.

3.3.6 Spindle Immersion

The spindle should be immersed up to the middle of the shaft indentation. Failure to do so could result in incorrect viscosity readings.

In some cases the sample fluid may change its rheological structure during the act of spindle immersion. To avoid this, we recommend inserting the spindle in a different portion of the sample than the one intended for measurement. The spindle may then be moved horizontally to the center of the sample container. This must be done before attaching the spindle to the Viscometer.

3.3.7 Sensitivity and Accuracy

Brookfield Viscometers are guaranteed to be accurate to within ± 1% of the full-scale range of the spindle/speed combination in use (this percentage, expressed in centipoise values, is equal to the spindle Factor; accuracy of a spindle/speed combination with a factor of 25 would therefore be within ± 25 cP). Repeatability is to within ± 0.2%.

The accuracy of a particular viscosity reading is dependent upon the actual dial or display reading. In general, accuracy of the viscosity value will increase as the reading approaches 100. This is because the tolerance of ± 1% of full-scale viscosity applies to all readings, and represents a smaller percentage of measured viscosity as the actual reading increases. Consider the following example:

An LVT Viscometer, when used with a #1 spindle at a speed of 60 RPM, has a spindle Factor of 1 (obtained from the Factor Finder supplied with each instrument). Since the full-scale range of any spindle/speed combination is equal to the Factor multiplied by 100, the full-scale viscosity range in this case is 100 cP. The accuracy tolerance is ± 1% of this range, or 1 cP, irrespective of the Viscometer's dial or display reading. Refer to the following table to see how this affects the accuracy of various readings taken with this spindle/speed combination:

Viscometer Reading	Viscosity	Possible Error	% Error
100	100 cP	1 cP	1%
50	50 cP	1 cP	2%
10	10 cP	1 cP	10%

The same principle applies to the repeatability of the reading. As with accuracy, the potential error introduced by the repeatability tolerance becomes less significant as the dial or display reading increases.

3.3.8 Obtaining a Viscometer Reading

Before operating the Viscometer, be sure that it is securely attached to its stand and has been properly leveled. Select a spindle and speed combination and attach the spindle to the Viscometer.

Turn the Viscometer on and allow it to run until a constant reading is obtained. Be prepared, however, for some overshoot since momentum gained by the spindle during acceleration may cause the reading to initially oscillate about the final equilibrium value.

A number of procedures can be employed to obtain a satisfactory reading. In some cases, as much as 5 minutes must be allowed for the reading to reach apparent equilibrium. Usually you can just wait until the reading appears relatively constant for a reasonable time.

A more repeatable procedure is to specify a definite number of spindle revolutions to be counted before taking a reading. Since the time required for a certain number of revolutions will differ significantly with the speed in use, an alternate method is to let the spindle rotate for a specified period of time.

You may find that the reading does not come to equilibrium but continues to oscillate. This is usually due to the presence of an elastic as well as a viscous component in the fluid. If the reading continually increases or decreases, the fluid is probably time-dependent and requires special techniques to be measured successfully. See Section 4.5.

The torque display on the Digital Viscometer may fluctuate by 0.1 or 0.2% even after equilibrium is reached. If this happens, simply use the median value as the accepted reading. Larger fluctuations may indicate the conditions described in the preceding paragraph.

Once a valid reading is obtained, multiply it by the Factor for the spindle/speed combination you are using. The Factor will be found on the Factor Finder supplied with the Viscometer.

A note about Factors and Ranges; both can be used to calculate viscosity from a given reading. A Factor (such as that obtained from the Factor Finder) is simply multiplied by the Viscometer reading to calculate viscosity (in centipoise). A Range (as sup-

plied with some Brookfield Accessories in lieu of a Factor) is equal to the Factor multiplied by 100. Therefore, to calculate viscosity, first divide the Range by 100, then multiply by the Viscometer dial or display reading.

3.3.9 A Calibration Check

People are often concerned about the accuracy of their Viscometer. Here are some tests of its mechanical performance:

(A) Variations in power frequency will cause the spindle to rotate at an incorrect speed. If you are in an area where electric clocks are used, this factor may be immediately eliminated. Voltage variations have no effect as long as the deviation is not greater than ± 10% of the nameplate voltage and the frequency remains constant.

Other readily apparent symptoms of improper power supply are: failure of the motor to start, jerky spindle rotation, a wildly fluctuating pointer, or inconsistent digital display readings.

(B) Damage to the pivot point or jewel bearing will adversely affect accuracy and repeatability of the Viscometer. The following Oscillation Test will allow you to evaluate the condition of these components:

1. The Viscometer should be mounted and leveled, with no spindle installed and the power switch in the "off" position for Dial Reading Viscometers; Digital Viscometers should have the power on, the motor off.
2. Turn the spindle coupling to deflect the pointer or digital display upscale from its zero position to a torque reading of 5 to 10 and let it swing back under its own power.
3. If the pointer swings freely and smoothly, and returns to zero each time this test is repeated, the pivot point and jewel bearing are in good condition. If it crawls back or sticks on the dial, performance of the Viscometer will not be up to specification, and it should be serviced. On Digital Viscometers the digital display should fluctuate smoothly and return to a zero reading.

(C) We have never found a spring made of beryllium copper which showed any change in its characteristics due to fatigue, even after hundreds of thousands of flexings. For this reason, a check of the calibrated spring is usually not necessary. There is no external zero adjustment on dial-reading models for the same reason. The zero adjustment on Digital models is provided to compensate for any possible heat-induced drift in the electronic circuitry.

(D) Use of a calibrated viscosity standard is recommended as a final performance check. Test the viscosity standard as you would any sample fluid, carefully following any applicable instructions. Brookfield Viscosity Standards (calibrated to within ±1%) are ideal for this test. The use of fluids other than viscosity standards is not recommended due to the probability of unpredictable rheological behavior.

(E) If the Viscometer passes all of the preceding tests, its performance should be satisfactory. Should accuracy or operation of the instrument still be suspect, please refer to the troubleshooting chart in Section 3.5.

3.3.10 Recalibrating the Brookfield Viscometer

In many cases it is not practical to use a 600 mL low form Griffin beaker when making measurements with a Brookfield Viscometer. It may be desirable to use a different container if transferring the material proves messy or time-consuming. Sometimes people also use the instrument without the guard leg to avoid the extra cleaning that would otherwise be involved. Either of these practices requires that a recalibration of the instrument be made if accurate results are to be obtained.

If measurements have been made under one set of conditions and you merely wish to establish a reference point with the same material under new conditions, the following procedure will suffice:

1. Measure the material in both the old and new container and/or with the guard leg removed and in place. Be sure that the same spindle and speed are used and that the temperature of the material remains the same.
2. Note the new reading - this is the new reference point corresponding to the original value.

This procedure may be used in establishing control methods to be followed when the Viscometer is to be used for quality control purposes, and the operator is not concerned with the actual centipoise value of the material.

If your work requires that actual centipoise values be obtained, we suggest the following procedure if a different container is to be used or if you don't wish to use the guard leg:

(1) Following the procedures outlined earlier in this chapter, measure the viscosity of a Newtonian fluid, using a standard container as specified in Section 3.3.4. Brookfield Viscosity Standards are highly recommended for this procedure. Perform this measurement carefully, as the accuracy of your end result depends upon it. Multiply the Viscometer reading by the appropriate Factor to determine the fluid's viscosity in centipoise.

(2) Transfer the Standard to the container for which the Viscometer is to be calibrated. Ensure that the fluid temperature is the same as it was during Step (1).

(3) Using the same spindle you intend to use for subsequent sample testing, measure vis-

cosity of the Standard in the new container. Note the dial or display reading and speed, S1.

(4) The new range of measurement is determined by this formula:

$$R1 = \frac{100\eta}{x}$$

Where R1 is the full-scale range of measurement under the new conditions; η is the viscosity of the Standard as measured in step (1); and x is the dial or display reading obtained in step (3).

(5) To calculate the resulting new ranges when the same spindle is operated at different speeds under the new conditions, use this formula:

$$\frac{R1}{R2} = \frac{S2}{S1}$$

Where R1 is the range already established in Step (4) for RPM of S1, and S2 is the speed for which range R2 is to be determined.

(6) The multiplying factor (f) for the new conditions can be determined by this formula:

$$f = \frac{R1}{100}$$

Where R1 is the range for the particular spindle and speed combination used, as determined in Step (4).

To calculate viscosity, therefore, multiply the reading obtained on the Viscometer's 0-100 scale by f.

3.4 Viscometer Maintenance

Brookfield Viscometers are highly reliable, provided the instrument is handled properly. Most problems are readily detected by the Calibration Check in Section 3.3.9. To prevent potential problems, a few pointers are worth remembering:

(A) The forces to which the Viscometer responds are extremely small; the optimum performance of the instrument depends on the elimination of all unnecessary friction which may affect its sensitivity. This means cleanliness. Care must be taken to prevent dust, fumes, liquids, and other forms of contamination from entering the Viscometer housing. If it is necessary to use the instrument in such environments, use of the spindle extensions and/or purge fittings is recommended to minimize the entry of contaminants. More information on these accessories can be found in Section 2.1.10.

(B) Never place the instrument upside down with a fluid-coated spindle attached.

(C) Do not expose the Viscometer to ambient temperatures in excess of 75°C. When measuring samples at high temperatures, the use of spindle extensions or the Thermosel accessory is recommended.

(D) Avoid applying side- or down-thrust to the spindle coupling; this protects the pivot point and jewel bearing, which can be broken or dulled by rough treatment. Always lift the spindle coupling when attaching or removing a spindle. Do not strike the spindle against the sample container or otherwise apply side-thrust to it. Do not pull down on the spindle or spindle coupling.

(E) Do not drop or severely jar the instrument. The Brookfield Laboratory Stand provides a convenient, sturdy support. If the Viscometer is intended for portable use, it should be stored in its carrying case when not in use.

If the Viscometer is physically damaged or fails the Oscillation Test in Section 3.3.9, it should be returned for repair to Brookfield Engineering Laboratories or to the dealer from whom it was purchased.

The need for periodic preventative maintenance varies with the conditions of use. Under normal circumstances, a yearly service should be sufficient to keep the Viscometer in top working order. More severe use will necessitate more frequent service. The instrument should be returned to Brookfield or one of its dealers for this service.

3.5 Viscometer Troubleshooting

Specific fault diagnosis procedures are detailed in the instruction manual that is provided with each Viscometer. The chart below lists some of the more common problems that you may encounter while using your Viscometer, along with the probable causes and suggested cures.

Spindle Does Not Rotate

- ❏ Make sure the viscometer is plugged in.
- ❏ Check the voltage rating on your viscometer (115V, 220V): it must match the wall voltage.
- ❏ Make sure the power switch is in the ON position.
- ❏ Make sure the speed selection is set properly and securely at the desired speed.

Spindle Wobbles When Rotating or Looks Bent

- ❏ Make sure the spindle is tightened securely to the viscometer coupling.
- ❏ Check the straightness of all other spindles; replace them if bent.
- ❏ Inspect viscometer coupling and spindle coupling mating areas and threads for dirt: clean threads on spindle coupling with a 3/56-inch left-hand tap.
- ❏ Inspect threads for wear; if the threads are worn, the unit needs service.
- ❏ Check to see if spindles rotate eccentrically or wobble. There is an allowable runout of 1/32-inch in each direction (1/16-inch total) when measured horizontally from the bottom of the spindle rotating in air.
- ❏ Check to see if the viscometer coupling is

bent; if so, the unit is in need of service.

If you are continuing to experience problems with your viscometer, follow this diagnosis section to help isolate the potential problem.

Perform an Oscillation Check

- ❏ Remove the spindle and turn the motor OFF.
- ❏ Gently push up on the viscometer coupling.
- ❏ Turn the coupling until the red pointer reaches 15-20 on the Dial Viscometer or the torque readings reach 15-20% on the Digital Viscometer.
- ❏ Gently let go of the coupling.
- ❏ Watch the pointer swing freely and finally rest on zero on the Dial Viscometer or the torque reading returns to zero on the Digital Viscometer.

If the pointer sticks or the torque reading does not return to zero, the unit is in need of service.

Perform a Calibration Check

- ❏ Verify spindle, speed and model selection
- ❏ Verify test parameters: temperature, container, volume, method.
- ❏ Perform a calibration check in accordance with the procedures from the viscometer operating manual
  - ♦ Verify tolerances are calculated correctly.
  - ♦ Verify calibration check procedures were followed exactly

If the unit is found to be out of tolerance, the unit is in need of service. Please follow the procedures outlined in the viscometer operating manual.

CHAPTER 4

4.1 Coming to Grips with Rheology

Rheology is defined by Webster's Dictionary as "the study of the change in form and the flow of matter, embracing elasticity, viscosity, and plasticity." We concern ourselves in this chapter with viscosity, further defined
as "the internal friction of a fluid, caused by molecular attraction, which makes it resist a tendency to flow." Your Brookfield Viscometer measures this friction, and therefore functions as a tool of rheology. The purpose of this chapter is to acquaint you with the different types of flow behavior and use of the Brookfield Viscometer as a rheological instrument to enable you to conduct a detailed analysis of virtually any fluid. This information is useful to all Viscometer users, particularly those adhering to the Theoretical and Academic schools of thought on viscosity measurement.

4.2 Viscosity

Viscosity is the measure of the internal friction of a fluid. This friction becomes apparent when a layer of fluid is made to move in relation to another layer. The greater the friction, the greater the amount of force required to cause this movement, which is called "shear." Shearing occurs whenever the fluid is physically moved or distributed, as in pouring, spreading, spraying, mixing, etc. Highly viscous fluids, therefore, require more force to move than less viscous materials.

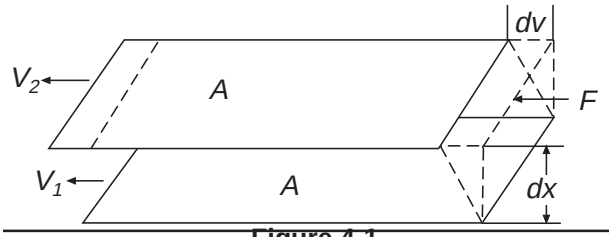


Figure 4-1

Isaac Newton defined viscosity by considering the model represented in Figure 4-1. Two parallel planes of fluid of equal area "A" are separated by a distance "dx" and are moving in the same direction at different velocities "V1" and "V2." Newton assumed that the force required to maintain this difference in speed was proportional to the difference in speed through the liquid, or the velocity gradient. To express this, Newton wrote:

$$\frac{F}{A} = \eta \frac{dv}{dx}$$

where η is a constant for a given material and is called its "viscosity'.

The velocity gradient, $\frac{dv}{dx}$, is a measure of the change in speed at which the intermediate layers move with respect to each other. It describes the shearing the liquid experiences and is thus called "shear rate." This will be symbolized as "S" in subsequent discussions. Its unit of measure is called the "reciprocal second" (sec^{-1}).

The term F/A indicates the force per unit arearequired to produce the shearing action. It is referred to as "shear stress" and will be symbolized by "F'." Its unit of measurement is "dynes per square centimeter" (dynes/cm^2).

Using these simplified terms, viscosity may be defined mathematically by this formula:

$$\eta = \text{viscosity} = \frac{F'}{S} = \frac{\text{shear stress}}{\text{shear rate}}$$

The fundamental unit of viscosity measurement is the "poise." A material requiring a shear stress of one dyne per square centimeter to produce a shear rate of one reciprocal second has a viscosity of one poise, or 100 centipoise. You will encounter viscosity measurements expressed in "Pascal-seconds" (Pa•s) or "milli-Pascal-seconds" (mPa•s); these are units of the Inter-

national System and are sometimes used in preference to the Metric designations. One Pascal-second is equal to ten poise; one milli-Pascal-second is equal to one centipoise.

Newton assumed that all materials have, at a given temperature, a viscosity that is independent of the shear rate. In other words, twice the force would move the fluid twice as fast.

As we shall see, Newton was only partly right.

4.3 Newtonian Fluids

This type of flow behavior Newton assumed for all fluids is called, not surprisingly, "Newtonian." It is, however, only one of several types of flow behavior you may encounter. A Newtonian fluid is represented graphically in Figure 4-2. Graph A shows that the relationship between shear stress (F') and shear rate (S) is a straight line. Graph B shows that the fluid's viscosity remains constant as the shear rate is varied. Typical Newtonian fluids include water and thin motor oils.

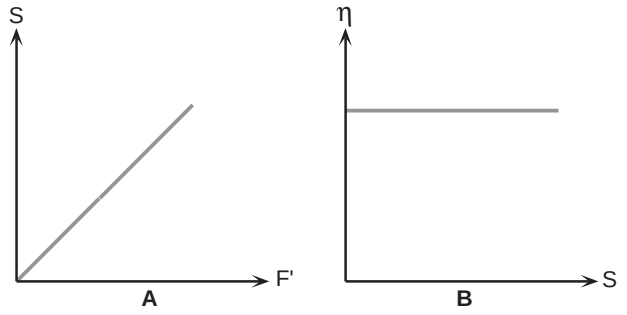


Figure 4-2

What this means in practice is that at a given temperature the viscosity of a Newtonian fluid will remain constant regardless of which Viscometer model, spindle or speed you use to measure it. Brookfield Viscosity Standards are Newtonian within the range of shear rates generated by Brookfield equipment; that's why they are usable with all our Viscometer models. Newtonians are obviously the easiest fluids to measure - just grab your Viscometer and go to it. They are not, unfortunately, as common as that much more complex group of fluids, the non-Newtonians, which will be discussed in the next section.

4.4 Non-Newtonian Fluids

A non-Newtonian fluid is broadly defined as one for which the relationship F'/S is not a constant. In other words, when the shear rate is varied, the shear stress doesn't vary in the same proportion (or even necessarily in the same direction). The viscosity of such fluids will therefore change as the shear rate is varied. Thus, the experimental parameters of Viscometer model, spindle and speed all have an effect on the measured viscosity of a non-Newtonian fluid. This measured viscosity is called the "apparent viscosity" of the fluid and is accurate only when explicit experimental parameters are furnished and adhered to.

Non-Newtonian flow can be envisioned by thinking of any fluid as a mixture of molecules with different shapes and sizes. As they pass by each other, as happens during flow, their size, shape, and cohesiveness will determine how much force is required to move them. At each specific rate of shear, the alignment may be different and more or less force may be required to maintain motion.

There are several types of non-Newtonian flow behavior, characterized by the way a fluid's viscosity changes in response to variations in shear rate. The most common types of non-Newtonian fluids you may encounter include:

PSEUDOPLASTIC: This type of fluid will display a decreasing viscosity with an increasing shear rate, as shown in Figure 4-3. Probably the most common of the non-Newtonian fluids, pseudoplastics include paints, emulsions, and dispersions of many types. This type of flow behavior is sometimes called "shear-thinning."

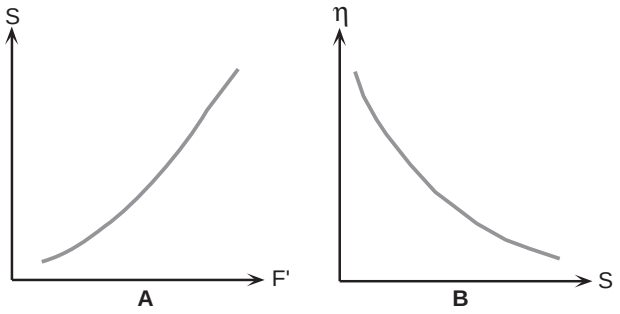


Figure 4-3

DILATANT: Increasing viscosity with an increase in shear rate characterizes the dilatant fluid; see Figure 4-4. Although rarer than pseudoplasticity, dilatancy is frequently observed in fluids containing high levels of deflocculated solids, such as clay slurries, candy compounds, corn starch in water, and sand/water mixtures. Dilatancy is also referred to as "shear-thickening" flow behavior.

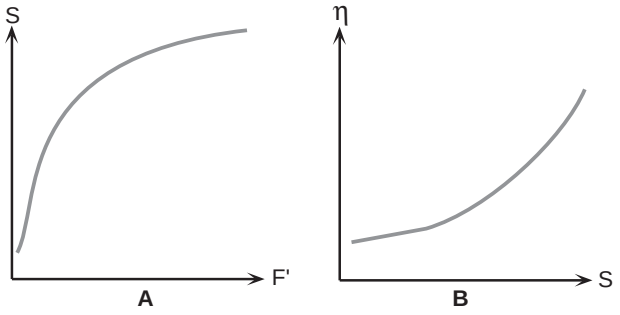


Figure 4-4

PLASTIC: This type of fluid will behave as a solid under static conditions. A certain amount of force must be applied to the fluid before any flow is induced; this force is called the "yield value." Tomato catsup is a good example of this type fluid; its yield value will often make it refuse to pour from the bottle until the bottle is shaken or struck, allowing the catsup to gush freely. Once the yield value is exceeded and flow begins, plastic fluids may display Newtonian, pseudoplastic, or dilatant flow characteristics. See Figure 4-5.

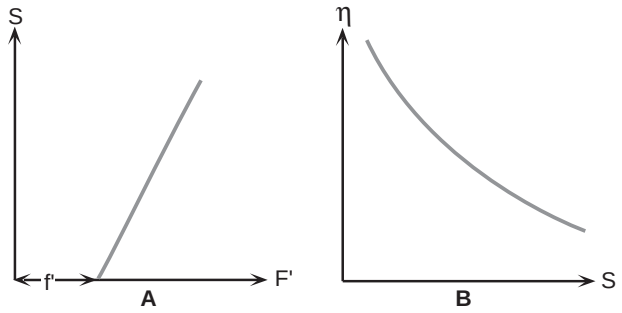


Figure 4-5

So far we have only discussed the effect of shear rate on non-Newtonian fluids. What happens when the element of time is considered? This question leads us to the examination of two more types of non-Newtonian flow: "thixotropic" and "rheopectic."

4.5 Thixotropy and Rheopexy

Some fluids will display a change in viscosity with time under conditions of constant shear rate. There are two categories to consider:

THIXOTROPY: As shown in Figure 4-6, a thixotropic fluid undergoes a decrease in viscosity with time, while it is subjected to constant shearing.

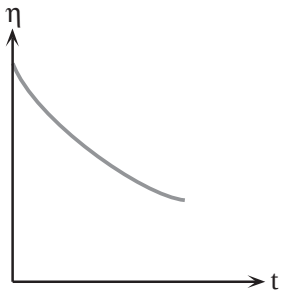


Figure 4-6

RHEOPEXY: This is essentially the opposite of thixotropic behavior, in that the fluid's viscosity increases with time as it is sheared at a constant rate. See Figure 4-7.

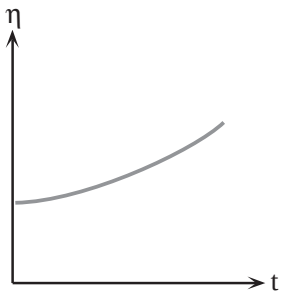


Figure 4-7

Both thixotropy and rheopexy may occur in combination with any of the previously discussed flow behaviors, or only at certain shear rates. The time element is extremely variable; under conditions of constant shear, some fluids will reach their final viscosity value in a few seconds, while others may take up to several days.

Rheopectic fluids are rarely encountered. Thixotropy, however, is frequently observed in materials such as greases, heavy printing inks, and paints.

When subjected to varying rates of shear, a thixotropic fluid will react as illustrated in Figure 4-8. A plot of shear stress versus shear rate was made as the shear rate was increased to a certain value, then immediately decreased to the starting point. Note that the "up" and "down" curves do not coincide. This "hysteresis loop" is caused by the decrease in the fluid's viscosity with increasing time of shearing. Such effects may or may not be reversible; some thixotropic fluids, if allowed to stand undisturbed for a while, will regain their initial viscosity, while others never will.

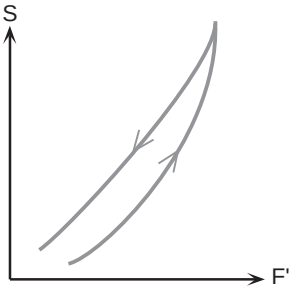


Figure 4-8

The rheological behavior of a fluid can, of course, have a profound effect on viscosity measurement technique. In Section 4.7 we will discuss some of these effects and ways of dealing with them. Chapter 5 will present advanced mathematical techniques used in analyzing flow behavior under a wide variety of conditions. First, however, we will discuss the effects of laminar and turbulent flow on viscosity measurement.

4.6 Laminar and Turbulent Flow

The very definition of viscosity implies the existence of what is called "laminar flow": the movement of one

layer of fluid past another with no transfer of matter from one to the other. Viscosity is the friction between these layers.

Depending on a number of factors, there is a certain maximum speed at which one layer of fluid can move with relation to another, beyond which an actual transfer of mass occurs. This is called "turbulence." Molecules or larger particles jump from one layer to another and dissipate a substantial amount of energy in the process. The net result is that a larger energy input is required to maintain this turbulent flow than a laminar flow at the same velocity.

The increased energy input is manifested as an apparently greater shear stress than would be observed under laminar flow conditions at the same shear rate. This results in an erroneously high viscosity reading.

The point at which laminar flow evolves into turbulent flow depends on other factors besides the velocity at which the layers move. A material's viscosity and specific gravity as well as the geometry of the Viscometer spindle and sample container all influence the point at which this transition occurs.

Care should be taken to distinguish between turbulent flow conditions and dilatant flow behavior (see Section 4.4). In general, dilatant materials will show a steadily increasing viscosity with increasing shear rate; turbulent flow is characterized by a relatively sudden and substantial increase in viscosity above a certain shear rate. The material's flow behavior may be Newtonian or non-Newtonian below this point.

Due to the relatively low shear rates at which most Brookfield Viscometers operate, it is unlikely that you will encounter turbulent flow unless you are measuring viscosities lower than 15 cP with an LV series Viscometer or 85 cP with other models. The higher the viscosity of a fluid, the less likely it is to experience turbulence. If turbulence is observed while measuring low viscosity fluids, it can often be eliminated by using the UL Adapter accessory (see Section 2.1.5).

4.7 What Affects the Rheological Property?

Viscosity data often functions as a "window" through which other characteristics of a material may be observed. Viscosity is more easily measured than some of the properties that affect it, making it a valuable tool for material characterization. Earlier in this chapter we discussed various types of rheological behavior and how to identify them. Having identified a particular rheological behavior in a material, you may wonder what this information implies about its other characteristics. This section, based on information gleaned from years of customer experience, is intended as a "tickler" to get you thinking about the mysteries your Viscometer can help you solve.

4.7.1 Temperature

One of the most obvious factors that can have an effect on the rheological behavior of a material is temperature. Some materials are quite sensitive to temperature, and a relatively small variation will result in a significant change in viscosity. Others are relatively insensitive. Consideration of the effect of temperature on viscosity is essential in the evaluation of materials that will be subjected to temperature variations in use or processing, such as motor oils, greases, and hot-melt adhesives.

4.7.2 Shear Rate

Non-Newtonian fluids tend to be the rule rather than the exception in the real world, making an appreciation of the effects of shear rate a necessity for anyone engaged in the practical application of rheological data. It would, for example, be disastrous to try to pump a dilatant fluid through a system, only to have it go solid inside the pump, bringing the whole process to an abrupt halt. While this is an extreme example, the importance of shear rate effects should not be underestimated.

When a material is to be subjected to a variety of shear rates in processing or use, it is essential to know its viscosity at the projected shear rates. If these are not known, an estimate should be made. Viscosity measurements should then be made at shear rates as close as possible to the estimated values.

It is frequently impossible to approximate projected shear rate values during measurement due to these values falling outside the shear rate range of the Viscometer. In this case, it is necessary to make measurements at several shear rates and extrapolate the data to the projected values. This is not the most accurate method for acquiring this information, but it is often the only alternative available, especially when the projected shear rates are very high. In fact, it is always advisable to make viscosity measurements at several shear rates to detect rheological behavior that may have an effect on processing or use. Where shear rate values are unknown or not important, a sample plot of viscosity versus RPM will often suffice.

Examples of materials that are subjected to, and are affected by, wide variations in shear rate during processing and use are: paints, cosmetics, liquid latex, coatings, certain food products, and blood in the human circulatory system. The following table shows typical examples of varying shear rates.

Situation	Typical range of shear rates (s^{-1})	Application
Sedimentation of fine powders in a suspending liquid	10^{-6} - 10^{-4}	Medicines, Paints
Levelling due to surface tension	10^{-2} - 10^{-1}	Paints, printing inks
Draining under gravity	10^{-1} - 10^{1}	Painting and coating, toilet bleaches
Extruders	10^{0} - 10^{2}	Polymers
Chewing and swallowing	10^{1} - 10^{2}	Foods
Dip coating	10^{1} - 10^{2}	Paints, confectionery
Mixing and stirring	10^{1} - 10^{3}	Manufacturing liquids
Pipe flow	10^{0} - 10^{3}	Pumping, blood flow
Spraying and brushing	10^{3} - 10^{4}	Spray-dying, painting, fuel atomization
Rubbing	10^{4} - 10^{5}	Application of creams and lotions to the skin
Milling pigments in fluid bases	10^{3} - 10^{5}	Paints, printing inks
High speed coating	10^{5} - 10^{6}	Paper
Lubrication	10^{3} - 10^{7}	Gasoline engines

4.7.3 Measuring Conditions

The condition of a material during measurement of its viscosity can have a considerable effect on the results of such measurement. It is therefore important to be aware of, and to control as much as possible, the environment of any sample you are testing.

First, the viscosity measurement techniques outlined in Section 3.3 should be adhered to. Variables such as Viscometer model, spindle/speed combination, sample container size, absence or presence of the guard leg, sample temperature, sample preparation technique, etc., all affect not only the accuracy of your measurements, but the actual viscosity of the material you are measuring.

Second, other less obvious factors that may affect viscosity must be considered. For example, the sample material may be sensitive to the ambient atmosphere, as is the case with dental impression materials, blast furnace, slag, blood and mucus. It may be that a controlled atmosphere favorable to the objectives of the test must be provided (see information on purge fittings in Section 2.1.10).

Another factor which may affect viscosity measurements is the homogeneity of the sample. It is usually desirable to have a homogeneous sample so that more consistent results may be obtained. Sometimes, however, tendency of a material to separate into non-homogeneous layers is the characteristic of most interest. Care must be taken in such instances not to disturb that which you wish to study by mixing or shaking the sample.

4.7.4 Time

The time elapsed under conditions of shear obviously affects thixotropic and rheopectic (time-dependent) materials. But changes in the viscosity of many materials can occur over time even though the material is not being sheared. Aging phenomena must be considered when selecting and preparing samples for viscosisty measurement. Consider also the fact that many materials will undergo changes in viscosity during the process of a chemical reaction, so that a viscosity measurement made at one time in the reaction may differ significantly from one made at another time.

4.7.5 Pressure

Variations in pressure may cause: dissolved gases to form bubbles; entrained gases to change size as well as distribution, and in some cases, turbulence. Pressure is not experienced as often as other parameters. Pressure compresses fluids, and thus, increases intermolecular resistance. Liquids are compressible under the influence of very high pressures - similar to gases but to a much lesser extent. Increases of pressure tend to increase the viscosity. As an example: The flow properties of highly concentrated slurries (above 70-80% by volume of particles) where there is insufficient liquid to fill completely all the voids between the particles results in a three-phase mixture (i.e. solids, liquids, and usually air). Due to the presence of air, the mixture is compressible, and therefore, the more you compress it, the greater the resistance to flow.

4.7.6 Previous History

What has happened to a sample prior to a viscosity measurement can significantly affect the result, especially in fluids sensitive to heat or aging. Thus, storage conditions and sample preparation techniques must be designed to minimize their effect on subsequent viscosity tests. Thixotropic materials in particular are sensitive to prior history, as their viscosity will be affected by stirring, mixing, pouring, or any other activity which produces shear in the sample.

4.7.7 Composition and Additives

The composition of a material is a determining factor of its viscosity. When this composition is altered, either by changing the proportions of the component substances, or by the addition of other materials, a change in viscosity is quite likely. For ex-

ample, the addition of solvent to printing ink reduces viscosity of the ink; and additives of many types are used to control the rheological properties of paints.

4.7.8 Special Characteristics of Dispersions and Emulsions

Dispersions and emulsions, which are multiphase materials consisting of one or more solid phases dispersed in a liquid phase, can be affected rheologically by a number of factors. In addition to many of the factors discussed previously, characteristics peculiar to multiphase materials are also significant to the rheology of such materials. These are discussed below.

One of the major characteristics to study is the state of aggregation of the sample material. Are the particles that make up the solid phase separate and distinct, or are they clumped together; how large are the clumps, and how tightly are they stuck together? If the clumps (flocs) occupy a large volume in the dispersion, viscosity of the dispersion will tend to be higher than if the floc volume was smaller. This is due to the greater force required to dissipate the solid component of the dispersion.

When flocs are aggregated in a dispersion, reaction of the aggregates to shear can result in shear-thinning (pseudoplastic) flow. At low shear rates, the aggregates may be deformed but remain essentially intact. As the shear rate is increased, the aggregates may be broken down into individual flocs, decreasing friction and therefore viscosity (For more information on pseudoplastic flow, see Section 4.4).

If the bonds within the aggregates are extremely strong, the system may display a yield value (see Section 4.4 about plastic flow). The magnitude of the yield value depends on the force required to break these bonds.

If a material's flocculated structure is destroyed with time as it is sheared, a time-dependent type of flow behavior will be observed (see Section 4.5).

If the shear rate is decreased after destruction of some or all of the flocculated structure, the material's viscosity may be lower than it previously was at the same shear rate. Since flocs begin to link together after destruction, the rate at which this occurs affects the time required for viscosity to attain previous levels. If the relinking rate is high, viscosity will be about the same as before. If the relinking rate is low, viscosity will be lower. This results in the rheological behavior called "thixotropy" (see Section 4.5).

The attraction between particles in a dispersed phase is largely dependent on the type of material present at the interface between the dispersed phase and the liquid phase. This in turn affects the rheological behavior of the system. Thus, the introduction of flocculating or deflocculating agents into a system is one method of controlling its rheology.

Shape of the particles making up the dispersed phase is also of significance in determining a system's rheology. Particles suspended in a flowing medium are constantly being rotated. If the particles are essentially spherical, rotation can occur freely. If, however, the particles are needle or plate-shaped, the ease with which rotation can occur is less predictable, as is the effect of varying shear rates.

The stability of a dispersed phase is particularly critical when measuring viscosity of a multiphase system. If the dispersed phase has a tendency to settle, producing a non-homogeneous fluid, the rheological characteristics of the system will change. In most cases, this means that the measured viscosity will decrease. Data acquired during such conditions will usually be erroneous, necessitating special precautions to ensure that the dispersed phase remains in suspension.

CHAPTER 5

5.1 Advanced Methods for Rheological Analysis

As mentioned in Chapter 1, those who follow the Academic school of thought on viscosity measurement have more complex needs than those who follow the Pragmatic or Theoretical schools. They need viscosity data that are defined in rheological terms. This usually requires a complete mathematical description of the Viscometer's operating parameters and an analysis of the rheological behavior of the fluid being studied.

Previous chapters have described various types of fluid behavior and their relationship to measurements made with Brookfield Viscometers and accessories. The Appendix details the significant operating parameters of this equipment and presents simplified formulas for obtaining shear rate and shear stress values. However, for many this information is still inadequate to perform the type of analysis they require. Having identified a particular flow behavior and defined it mathematically, these people need more information to understand how the fluid will react in a certain situation, and how to control that reaction. If is for these people that this chapter is provided.

In it you will find basic formulas from which the

simplified shear rate and shear stress information in the Appendix was derived. Also, various methods for analyzing Newtonian and non-Newtonian fluids are presented. The information presented here represents a cross-section of the most useful methods developed both by Brookfield Engineering Laboratories and by others. Other specific methods, usually applicable to a particular rheological problem, are sometimes available. Please inquire if you need more information.

5.2 Defining Operating Parameters of Various Spindle Geometries

In this section we present equations that define the operating parameters of spindle geometries found on various Brookfield Viscometers and accessories. These are organized according to the type of geometry being discussed. Definitions and values not listed may be found in the Appendix A.

5.2.1 Cylindrical Spindles

The following equations apply to cylindrical spindles only, used without a guard leg on any model Brookfield Viscometer.

SHEAR RATE (sec $^{-1}$): $$S = \frac{2\omega R_c^2 R_b^2}{x^2 (R_c^2 - R_b^2)} \quad (1)$$

SHEAR STRESS (dynes/cm^2): $$F' = \frac{M}{2\pi R_b^2 L} \quad (2)$$

VISCOSITY (poise): $$\eta = \frac{F'}{S} \quad (3)$$

Definitions:
- ω = angular velocity of spindle (rad/sec) [$= \left(\frac{2\pi}{60}\right) N$], N = RPM
- R_c = radius of container (cm)
- R_b = radius of spindle (cm)
- x = radius at which shear rate is being calculated
- M = torque input by instrument (see Appendix A)
- L = effective length of spindle (see Appendix A)

Note: R_c should not exceed $2R_b$ for well defined shear rates.

5.2.2 Coaxial Cylinders

Coaxial cylinder geometry is found in the UL Adapter, Small Sample Adapter, Thermosel System, DIN Adapter, Spiral Adapter and PVS Rheometer.

SHEAR RATE (sec $^{-1}$): $$S' = \left(\frac{2R_c^2}{R_c^2 - R_b^2}\right)\omega \quad (4)$$

SHEAR STRESS (dynes/cm^2): $$F' = \frac{M}{2\pi R_b^2 L} \quad (5)$$

VISCOSITY (poise): $$\eta = \frac{F'}{S'} \quad (6)$$

Definitions:
- S' = shear rate at surface of spindle (sec $^{-1}$)

See Section 5.2.1 for other definitions

5.2.3 Cone and Plate

These equations may be used with all models of the Wells-Brookfield Cone/Plate Viscometer and CAP Viscometer.

SHEAR RATE (sec $^{-1}$): $$S' = \frac{\omega}{\sin\theta} \quad (7)$$

SHEAR STRESS (dynes/cm^2): $$F' = \frac{M}{\frac{2}{3}\pi r^3} \quad (8)$$

VISCOSITY (poise): $$\eta = \frac{F'}{S'} \quad (9)$$

Definitions:
- θ = cone angle (degrees)
- r = cone radius (cm)

See Section 5.2.1 for definitions of other variables.

5.2.4 Disc and T-Bar Spindles

The standard disc-type spindles provided with most Viscometer models and the T-bar spindles used with the Helipath Stand accessory, as well as spindles with special shapes other than cylindrical or cone configurations, do not have directly definable shear rate and shear stress values. You may occasionally see the Viscometer's rotational speed referred to as a "shear rate," particularly when T-bar spindles are used. This is incorrect, as mathematical models are not available for calculating viscosity functions using T-bar spindles. However, models are available for the disc spindles. Refer to Technical Paper AR-82, available from Brookfield Engineering Laboratories.

5.2.5 Spiral Adapter Spindle

The Spiral Adapter has an inner, threaded spindle surrounded by a concentric outer cylinder. This combination causes the sample to be continually pumped up through the Spiral Adapter. The material reaches a steady state of flow during which viscosity is measured. The approximate shear rate in reciprocal seconds is .667N, where "N" is spindle speed in RPM.

5.2.6 "Paddle" / "Paste" Spindles

The Brookfield KU-1+ Viscometer uses a "paddle" spindle to measure the reaction torque when rotated at 200 RPM. Unlike "regular" viscometer spindles, the resultant viscosity is in KU (Krebb Units) and g (grams). Because of the unique spindle shape, no shear rate calculation is possible.

A paste spindle is available as an option to the paddle spindle. This spindle is similar to the paddle-type. The design consists of off-set rod-type vanes, approximately 22 mm x 19 mm long. The resultant viscosity is recorded in units of g (grams). It is suitable for use with high consistency materials such as roller mill pastes.

5.2.7 Other Special Spindles

Brookfield can produce special spindles upon request. This activity is coordinated through the Sales Department at Brookfield. Special spindles that have come out of this type of activity include vane-type spindles and special modifications of the Helipath Stand T-bars (i.e. multiple tines).

5.3 Analyzing Time-Independent Non-Newtonian Fluids

The equations we have presented thus far will yield precisely defined viscosity data for both Newtonian and non-Newtonian fluids. With Newtonian fluids, this is all the analysis that is necessary, since variations in shear rate will have no effect on viscosity of the fluid.

When the fluid is non-Newtonian, however, the situation is more complicated. While the equations permit complete definition of a reading made with a certain spindle at a certain speed, the numbers obtained with another spindle and/or speed will most likely be different. Which set of numbers is the 'right" one? Both, and neither! These differing numbers are part of the rheological description of the fluid, and therefore must be considered in the course of its analysis. In this section we will outline several methods for doing this on time-independent fluids as defined in Section 4.4.

5.3.1 Ratio Methods

A common method for characterizing and quantifying non-Newtonian flow is to figure the ratio of the fluid's viscosity as measured at two different speeds (with the same spindle). These measurements are usually made at speeds that differ by a factor of 10 (for example, 2 and 20 RPM, 10 and 100 RPM, etc.), but any factor may be established.

In constructing the ratio, the viscosity value at the lower speed should be placed in the numerator, the one at the higher speed in the denominator. Therefore, for pseudoplastic (shear thinning) fluids, the ratio will exceed 1.0 as the degree of pseudoplastic behavior increases. Conversely, for dilatant (shear thickening) fluids, the ratio will be less than 1.0 as the degree of dilatancy increases.

This procedure is commonly known as the "thixotropic index." The name is misleading since this ratio quantifies time-independent non-Newtonian behavior, not thixotropy, which is a time-dependent phenomenon. Analysis of time-dependent properties is detailed in Section 5.4.

A similar method eliminates calculation of viscosity and simply utilizes dial/display readings to derive what is known as a "viscosity ratio":

$$\text{VISCOSITY RATIO} = -\log\left(\frac{Mx}{M10x}\right) \qquad (10)$$

Definitions:
- Mx = Viscometer reading at speed x
- M10x = Viscometer reading at speed 10x (other ratios may be used)

5.3.2 Graphic Methods

The most basic graphic method of analyzing non-Newtonian flow is constructing a plot of viscosity versus spindle speed (using the same spindle for all readings.). Generally, viscosity is plotted along the Y-axis and speed (RPM) along the X-axis. Slope and shape of the resulting curve will indicate the type and degree of flow behavior. For examples of this type graph, see the illustrations accompanying the discussion of non-Newtonian flow types in Section 4.4.

Another method is to plot Viscometer reading (on the X-axis) as a function of speed (on the Y-axis). If the graph is drawn on log-log paper, the result is frequently a straight line. When this happens, the slope of the line (indicating the type and degree of non-Newtonian flow) and its intercept with the X-axis (indicating its yield value, if any) can be used as empirical constants.

When shear rate and shear stress are known, as with cylindrical spindles or coaxial cylinder geometry, these values may be substituted for speed and Viscometer reading in the above methods. Thus, predictions of viscosity at other shear rates may be made by interpolating between or extrapolating beyond the values available with a particular spindle geometry.

When using these methods with disc spindle geometries, it is best to plot speed on the Y-axis and to make all measurements with the same

spindle. An assumption that can be made with regard to shear rate is that, for a given spindle, the shear rate is proportional to the speed. Therefore the shear rate at 30 RPM (for example) is 10 times the shear rate at 3 RPM.

5.3.3 Template Method

A more sophisticated technique for the analysis of non-Newtonian fluids involves use of a "template." Its use is limited to fluids that follow the "power law," meaning ones that display one type of non-Newtonian flow, rather than shifting from one type to another as shear rate is varied. For example, a material that changed from pseudoplastic to dilatant flow when a certain shear rate is exceeded would not follow the power law over the full range of shear rates measured.

The template method is usable only with data generated with cylindrical spindles or coaxial cylinders. The data is fitted to a template to determine a constant called the STI." The STI is a convenient way to characterize non-Newtonian flow, much like the Viscosity Index. Certain parameters of the Viscometer in use and the STI are fitted to a second template, which is then used to predict the fluid's viscosity at any selected shear rate.

This is a useful method for predicting viscosity at shear rates not attainable by the Brookfield Viscometer, and for characterizing fluid behavior under a specific set of conditions. A complete description of the template method, including both templates, is available from Brookfield Engineering Laboratories as Technical Paper #AR-49.

5.3.4. Yield Value Determination

Some fluids behave much like a solid at zero shear rate. They will not flow until a certain amount of force is applied, at which time they will revert to fluid behavior. This force is called the "yield value" and measuring it is often worthwhile. Yield values can help determine whether a pump has sufficient power to start in a flooded system, and often correlate with other properties of suspensions and emulsions. The pourability of a material is directly related to its yield value.

A simple method for determining a relative yield value is to calculate the Brookfield Yield Value" using this ratio:

$$\text{YIELD VALUE} = \frac{Va - Vb}{100} \qquad (11)$$

Definitions:
- Va = Viscosity @ slowest available Viscometer speed
- Vb = Viscosity @ next-to-slowest Viscometer speed

With this method, Newtonian fluids will show a yield value of 0, while plastic fluids will show an increasing yield value as the predicted viscosity at zero shear increases.

A more accurate method of determining yield value involves plotting Viscometer readings on the X-axis versus speed (RPM) on the Y-axis on standard graph paper. The line thus obtained is extrapolated to zero RPM. The corresponding value for the Viscometer reading represents the yield value. If a cylindrical spindle is used to make the readings, the yield value may be calculated from this equation:

$$\text{YIELD VALUE} \quad \psi = x1 \bullet fa \qquad (12)$$

Definitions:
- y = yield value (dynes/cm^2)
- x1 = Viscometer reading @ 0 RPM
- fa = constant from table below

Cylindrical Spindle	Model LV	RV	HA	HB
1	0.16	1.72	3.44	13.78
2	0.67	7.11	14.21	56.85
3	2.56	27.30	54.60	218.39
4	12.48	133.14	266.28	1065.14
5	25.26	269.45	538.91	2155.63

Extrapolating the line to zero RPM is easy if the line is fairly straight. This is called Bingham flow. If the line is curved, as in pseudoplastic or dilatant flow, an estimate of X1 must be made by continuing the curve until it intersects the X-axis (0 on the Y-axis). This estimated value of X1 is then subtracted from all the other readings that comprise the graph. These new values are plotted on log-log paper, Viscometer reading versus speed. This graph will usually be a straight line for power law fluids if the value for X1 was estimated accurately. A curved line on this graph indicates that another estimate of X1 should be made.

Once a straight line is obtained the angle this line forms with the Y-axis (RPM) is measured. The power law index of this fluid can then be calculated from this equation:

$$\text{POWER LAW INDEX} \quad \overline{N} = \tan\theta \qquad (13)$$

Definitions:
- θ = Angle formed by plot line with Y-axis of graph

If θ is less than 45 degrees, the fluid is pseudoplastic; greater than 45 degrees, dilatant.

The power law index can be used to calculate the

effective shear rate at a given speed by using this equation:

SHEAR RATE
(sec^{-1}): $$S' = \frac{\overline{N}}{(0.2095)N} \quad (14)$$

Definitions: $\overline{N}$ = Power law index
N = Viscometer speed (RPM)

Another method for determining yield value and plastic viscosity when a plot of Viscometer reading versus speed produces a curved line is to plot the square root of the shear stress versus the square root of the shear rate. This often straightens the line and facilitates extrapolation to zero shear rate. This method is most suitable for pseudoplastic fluids with a yield value conforming to a model of flow behavior known as the Casson equation. More information is available from Brookfield Engineering Laboratories in Technical Papers AR-77 and AR-79.

5.4 Analyzing Time-Dependent, Non-Newtonian Fluids

In most cases, analysis of thixotropic and rheopectic fluids (see Section 4.5) involves plotting changes in viscosity as a function of time. The simplest method is to select a spindle and speed (preferably a low speed) and leave the Viscometer running for an extended period, noting the dial or display reading at regular intervals. It is important to control temperature of the sample fluid carefully so that variations in temperature won't affect the results. A change in the fluid's viscosity over time indicates time-dependent behavior; a decrease signifies thixotropy, an increase rheopexy (or, in some cases, curing of the sample material).

A second method is to graph the Viscometer reading versus speed, using a single spindle. Starting at a low speed, note the reading at each successively higher speed until the reading goes off scale. A graph of these readings is the "up curve." Without stopping the Viscometer, reduce the speed incrementally to the starting point, again noting the reading at each speed. This is the "down curve." It is best to allow a consistent time interval between each speed change. If the fluid is time-independent, the "up curve" and the "down curve" will coincide. If they do not, the fluid is time-dependent. Position of the "up curve" and the "down curve" indicates the type of flow behavior: if the "up curve" indicates a higher viscosity than the "down curve," the fluid is thixotropic; lower, rheopectic.

An indication of the recovery time of the fluid (how quickly it returns to its initial viscosity after exposure to shear conditions) can be obtained by turning off the Viscometer at the end of the "down curve," waiting for a given period of time, restarting the Viscometer and immediately taking a reading.

A more sophisticated approach is to calculate the "thixotropic breakdown coefficient." This is a single number which quantifies the degree of thixotropy (or rheopexy) displayed by the sample fluid. First, plot Viscometer reading (using a specified spindle/speed combination) versus log time, taking readings at regular intervals. This usually produces a straight line. Then, apply the following equation:

THIXOTROPY BREAKDOWN COEFFICIENT:

$$Tb = \left(\frac{St_1 - St_2}{\ln\left(\frac{t_2}{t_1}\right)} \right) \bullet F \quad (15)$$

Definitions: St_1 = Viscometer reading at t_1 minutes
St_2 = Viscometer reading at t_2 minutes
F = Factor for spindle/speed combination

Plots of thixotropic behavior may sometimes be used to predict the gel point of a fluid. One way to do this is to plot log Viscometer reading versus time, using a single spindle and speed. If the resulting line has a steep slope, gelling is likely to occur. If the line curves and flattens out, gelation is unlikely.

Another technique is to plot time versus the reciprocal of the Viscometer reading. In this method, the gel point can be read from the curve intercept at a Viscometer reading of 100. Fluids which do not gel will be asymptotic to the vertical axis.

5.5 Temperature Dependence of Viscosity

The viscosity of most fluids decreases with an increase in temperature. By measuring viscosity at two temperatures (using a single spindle and speed), it is possible to predict a flow curve representing the temperature dependence of the viscosity of a fluid according to the following relationships using the application of simultaneous equations:

$$\eta = A \bullet e^{\left(\frac{B}{T}\right)} \quad (16)$$

$$\text{where } B = \left(\frac{T_1 \bullet T_2}{T_1 - T_2}\right) \bullet \ln\left(\frac{\eta_2}{\eta_1}\right)$$

$$A = \eta_1 \bullet e^{\left(\frac{-B}{T_1}\right)}$$

Definitions: T_1 = Temperature at which viscosity η_1 was measured
T_2 = Temperature at which viscosity η_2 was measured

There are many other techniques available for analyzing the rheological behavior of fluids under a variety of conditions. Space doesn't permit a detailed discussion here, but more information can be obtained from Brookfield Engineering Laboratories on these and other advanced methods:

- Approximation of shear rate and shear stress values using disc type spindles (AR-82).
- Techniques for determination of extremely low-shear viscosity and leveling behavior of coating materials using "spring relaxation" procedures (AR-84).
- Computer analysis of certain rheological characteristics.

Math Models

The analysis of viscometer data may be enchanced through the use of mathematical models. Non-Newtonian behavior can be simply expressed through an equation, and in some cases, the coefficients of a model can be used to infer performance of a fluid under conditions of use.

Newtonian flow is defined by a proportional response in shear stress for a change in shear rate (a linear relationship). Non-Newtonian fluids will exhibit a non-linear stress/rate relationship. Newton's equation for viscosity has been modified many times to attempt to characterize non-Newtonian behavior. Some of the more widely used equations include Bingham, Casson, NCA/CMA Casson and Power Law.

Bingham

$$\tau = \tau_o + \eta D$$

Casson

$$\sqrt{\tau} = \sqrt{\tau_o} + \sqrt{\eta D}$$

NCA/CMA Casson

$$(1+\alpha)\sqrt{\tau} = 2\sqrt{\tau_o} + (1+\alpha)\sqrt{\eta D}$$

Power Law

$$\tau = kD^n$$

where: τ = shear stress
D = shear rate
η = viscosity
τ_o = yield stress
k = consistency index
n = flow index
α = aspect ratio

The chocolate industry utilitzes the NCA/CMA version of the Casson equation to evaluate chocolate prior to final processing. This equation closely approximates the plastic behavior of chocolate. In addition, experience shows that the slope term, $\sqrt{\eta}$ (plastic viscosity), indicates the chocolate's response to being moved in processing (mixing, pumping). Also, the "y" intercept, $2\sqrt{\tau_0}$ (yield stress or zero shear viscosity), indicates the force required to start/stop flowing (molding, enrobing). A particular batch of chocolate can be modified to achieve the specific performance characteristics required for the next processing step.

The oil drilling industry in the United States utilizes the power law equation to evaluate the performance of drilling mud and fracturing fluid. The latter is a material forced into a non-performing well to allow for additional oil recovery. The power law equation has been found to closely approximate its pseudoplastic behavior. In addition, experience shows that the power term (*n*, flow index) indicates the ability of the fluid to be moved down into the well. The coefficient (*k*, consistency index) indicates low shear rate flow behavior of the mud once it is at the far reaches of the well. A fracturing fluid can be modified in its storage vessel to obtain the appropriate flow characteristics prior to being pumped into the well.

In both cases described above, the successful use of the math model will prevent the utilization of improper fluid, and ultimately, poor performance or rejected material. The math model should be utilized as a tool to better understand and interpret viscometer data.

The utilization of math models normally requires viscosity data collection under defined conditions of shear rate and shear stress. Many spindle geometries are available for use with your Brookfield Viscometer/Rheometer which will provide shear stress and shear rate data. In addition, Brookfield offers several software packages and some instruments with the embedded capability to analyze data sets using a variety of mathematical models. Our brochure "Technical Papers on Viscosity Measurement and Control" lists available papers on specific application areas as well as general-interest experimental techniques. If you don't have the current edition, let us know and we'll send one to you. Ask for Data Sheet 091-C.

5.7 Brookfield Application Software

Brookfield offers various software programs which work in conjunction with viscometers/rheometers to allow for automatic data collection, analysis including use of math models and the creation of permanent test records:

Software	Instrument Required
RHEOCALC	DV-III+ Rheometer
WINGATHER	DV-II+ Viscometer
CAPCALC	CAP series Viscometers
RHEOVISION	PVS Rheometer

APPENDIX A: Specifications,

Ranges, and Operating Parameters

This Appendix is intended to provide the user of Brookfield Viscometers and accessories with all the information required to perform mathematical analyses of viscosity data acquired with this equipment. It includes essential dimensions, range tables and constants, organized by product in data sheet form. The following Brookfield Viscometers and accessories are covered:

Calibration Spring Torque for Standard Dial-Reading Viscometer and Digital Viscometer/Rheometer

LV	673.7 dyne-centimeters (full scale)
RV	7187.0 dyne-centimeters (full scale)
HA	14,374.0 dyne-centimeters (full scale)
HB	57,496.0 dyne-centimeters (full scale)

Notes:
1. These values apply to all models with the same prefix designation: LV refers to LVF, LVT, LVTD, LVT-CP, LVTDCP, etc.
2. For intermediate models multiply the base spring torque by the multiplier in the model designation: 5XLVT = 5 X 673.7 = 3368.5 dyne-centimeters (full scale). Multiplier also applies to all Factors and ranges.
3. Torque at any dial or display reading equals reading multiplied by full-scale torque divided by 100: RVT model, reading 40; torque = (40 X 7187.0)/100 = 2874.8 dyne-cm.

A note about the terms appearing in this Appendix:

Shear rate constants (where given) are simply multiplied by the Viscometer's rotational speed (in RPM) to obtain the shear rate (in reciprocal seconds) for that speed. The constants are independent of Viscometer model, sample viscosity, or temperature.

Spindle factors are listed as constants related to the Viscometers rotational speed. Divide the constant by the speed in use to obtain the Factor for that spindle/speed/Viscometer model combination. This Factor is then multiplied by the Viscometer's dial or display reading to obtain viscosity (in centipoise).

For example: the Factor for a #2 LV spindle on an LV Viscometer is given as 300/N (Section A.1.4). The Viscometer's rotational speed (RPM) is represented by N. If the measurement is being made at 12 RPM, the Spindle Factor is 300/12, or 25. Multiply all Viscometer readings made with this spindle/speed combination by 25 to obtain viscosity in centipoise.

Where given, Sample Chamber Diameter refers to inside diameter (I.D.). Spindle Diameters are outside diameters (O.D.).

All dimensions are given in inches and in millimeters (in parentheses) unless otherwise noted. Be sure to use the metric values when required for rheological equations.

A.1 Dial-Reading Viscometer Spindles and Speeds

Model	No. of Spindles	No. of Speeds	Speeds (rpm)
LVF	4	4	60, 30, 12, 6
LVT	4	8	60, 30, 12, 6, 3, 1.5, 0.6, 0.3
RVF	7	4	20, 10, 4, 2
RVF-100	7	4	100, 50, 20, 10
RVT	7	8	100, 50, 20, 10, 5, 2.5, 1, 0.5

Notes:
1. Speed variations (other than standard models listed above) are identified by suffix in model designation: RVT-200 fastest speed is 200 RPM. All other speeds are in same proportion as standard models: RVT-200 speeds are 200, 100, 40, 20, 10, 5, 2, 1 RPM.
2. RPM specifications apply to all Viscometers with same model designation: LVT refers to LVT, LVTD, LVT-CP, LVTDCP, etc. (each of these instruments has eight speeds as shown above for LVT model).
3. Check with factory regarding availability of non-standard calibration spring torques and rotational speeds.

A.2 Digital Viscometers/Rheometers Spindles and Speeds

Viscometer/ Rheometer	No. of Spindles	No. of Speeds	Speeds (rpm)
LV DV-E	4	18	100, 60, 50, 30, 20, 12, 10, 6, 5, 4, 2.5, 2, 1, .6, .5, .3
RV/HA/HB DV-E	7	18	100, 60, 50, 30, 20, 12, 10, 6, 5, 4, 2.5, 2, 1, .6, .5, .3
LV DV-I+	4	18	100, 60, 50, 30, 20, 12, 10, 6, 5, 4, 2.5, 2, 1, .6, .5, .3
RV/HA/HB DV-I+	7	18	100, 60, 50, 30, 20, 12, 10, 6, 5, 4, 2.5, 2, 1, .6, .5, .3
LV DV-II+	4	54	.01 to 200 rpm
RV/HA/HB DV-II+	7	54	.01 to 200 rpm
LV DV-III+	4	2,600	.01 to 250 rpm (.1 rpm increments from 0.1 to 250)
RV/HA/HB DV-III+	7	2,600	.01 to 250 rpm (.1 rpm increments from 0.1 to 250)

A.3 Disc Spindles for Dial-Reading Viscometers and Digital Viscometers/Rheometers

Disc Spindle Factors

Spindle	LV	RV	HA	HB
#2 LV	300/N*	—	—	—
#3 LV	1200/N	—	—	—
#1 RV/H	—	100/N	200/N	800/N
#2 RV/H	—	400/N	800/N	3200/N
#3 RV/H	—	1000/N	2000/N	8000/N
#4 RV/H	—	2000/N	4000/N	16M/N
#5 RV/H	—	4000/N	8000/N	32M/N
#6 RV/H	—	10M/N	20M/N	80M/N

*N = RPM M = 1000

Disc Spindle Dimensions

Spindle	Figure	C-Diameter	D	E	F
#2 LV	1	.7370 (18.72)	.270(6.86)	1.000(25.4)	1.969 (50.0)
#3 LV	1	.4970 (12.6)	.070 (1.78)	1.007 (25.6)	1.969 (50.0)
#1 RV	2	2.2150 (56.26)	.885 (22.48)	1.062 (26.97)	2.406 (61.12)
#1 H	2	2.2150 (56.26)	.908 (23.06)	1.062 (26.97)	2.406 (61.12)
#2 RV	3	1.8477 (46.93)	.0565 (1.65)	1.062 (26.97)	1.938 (49.21)
#2 H	3	1.8550 (47.12)	.065 (1.65)	1.062 (26.97)	1.938 (49.21)
#3 RV/H	3	1.3658 (34.69)	.065 (1.65)	1.062 (26.97)	1.938 (49.21)
#4 RV/H	3	1.0748 (27.3)	.065 (1.65)	1.062 (26.97)	1.938 (49.21)
#5 RV/H	3	.8324 (21.14)	.065 (1.65)	1.062 (26.97)	1.938 (49.21)
#6 RV/H	1	.5757 (14.62)	.062 (1.57)	1.188 (30.17)	1.938 (49.21)

Dimensions are in inches (mm). Dimension A is 4.531 (115) on LV spindles; 5.250 (133) on RV/H spindles. Dimension B is .125 (3.2) on all spindles.

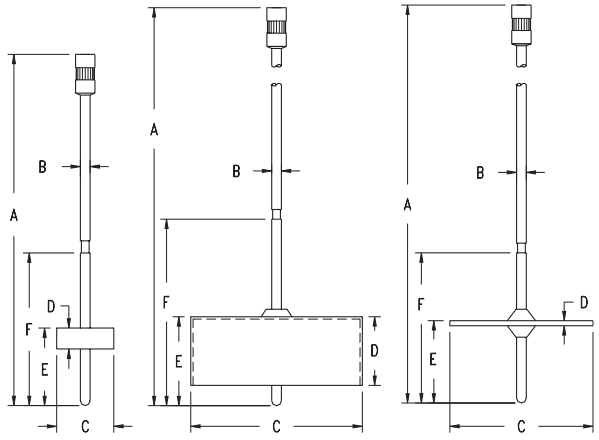


Fig. 1 **Fig. 2** **Fig. 3**

A.4 Cylindrical Spindles for Dial-Reading Viscometer and Digital Viscometers/Rheometers

Cylindrical Spindle Factors and Shear Rates

Spindle	LV	RV**	HA**	HB**	Shear Rate (sec^{-1})
#1 LV	60/N*	780/N	1560/N	6240/N	0.220N
#2LV CYL	300/N	3350/N	6700/N	26.8M/N	0.212N
#3 LV CYL	1200/N	12.9M/N	25.8M/N	103.2M/N	0.210N
#4 LV	6000/N	64M/N	128M/N	512M/N	0.209N
#5 LV CYL +	12M/N	128M/N	256M/N	1024M/N	0.209N
#7 RV/H	3750/N	40M/N	80M/N	320M/N	0.209N

*N = RPM M = 1000 + = Optional Item
**Factors are for readings made without using the guardleg.

Cylindrical Spindle Dimensions (for equations used in 5.2.1, see "Cylindrical Spindle Equation Table" on the following page.

Spindle	Figure	C-Diameter	D	F
#1 LV	1	.7418(18.84)	2.563(65.1)	3.188(80.97)
#2 LV CYL	1	.4037(10.25)	2.124(53.95)	2.624(66.65)
#3 LV CYL	2	.2315(5.88)	1.688(42.86)	2.094(53.19)
#4 LV	3	.1250(3.2)	1.221(31.01)	.375(9.53)
#5 LV	3	.1250(3.2)	0.596(15.14)	.375(9.53)
#7 RV/H	3	.1250(3.2)	1.983(50.37)	.375(9.53)

Dimensions are in inches (mm). Dimension A is 4.531 (115) on LV spindles; 5.250 (133) on RV/H spindles.
Dimension B is .125 (3.2) on all spindles.

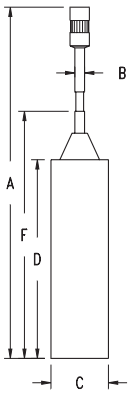


Fig. 1

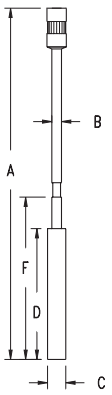


Fig. 2

Fig. 3

The following cylindrical spindle table depicts information for *use with the equations presented in 5.2.1.* only.

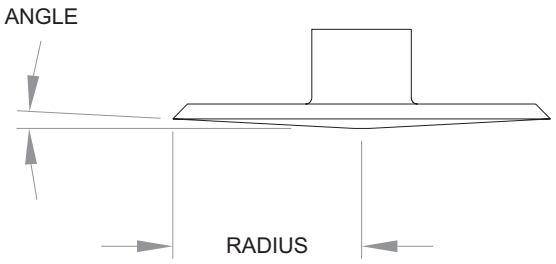
Cylindrical Spindle Equation

Spindle	Figure	C-Diameter	D	F
#1 LV	1	.7418(18.84)	2.563(65.1)	3.188(80.97)
#2 LV CYL	1	.4037(10.25)	2.124(53.95)	2.624(66.65)
#3 LV CYL	2	.2315(5.88)	1.688(42.86)	2.094(53.19)
#4 LV	3	.1250(3.2)	1.221(31.01)	.375(9.53)
#5 LV	3	.1250(3.2)	0.596(15.14)	.375(9.53)
#7 RV/H	3	.1250(3.2)	1.983(50.37)	.375(9.53)

*Effective length includes correction for end effect and should be used in equations. Actual length is given for reference only.

A.5 Wells-Brookfield Cone/Plate Viscometer Factors, Dimensions and Shear Rates

Cone Spindle Dimensions and Shear Rates



Cone Spindle	Angle (degrees)	Radius (cm)	Sample Size (mL)	Shear Rate (sec^{-1})
CP40	0.8	2.4	0.5	7.5N*
CP-42	3.0	2.4	2.0	2.0N
CP-42	1.565	2.4	1.0	3.84N
CP-51	1.565	1.2	0.5	3.84N
CP-52	3.0	1.2	0.5	2.0N

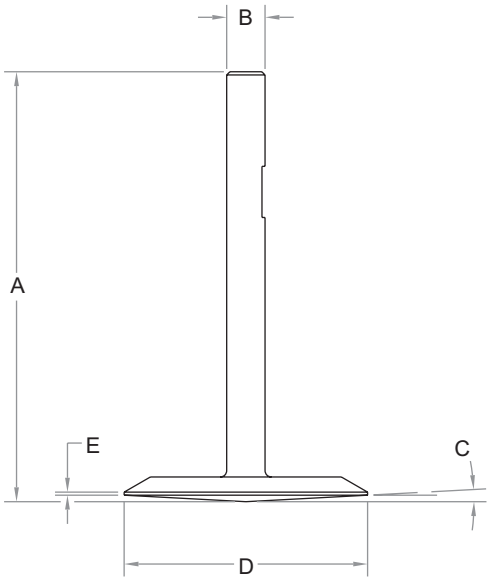
*N = RPM

Cone Spindle Factors

Cone Spindle	LV	RV	HB
CP-40	3.07/N*	32.7/N	261.6/N
CP-41	11.51/N	122.88/N	982.4/N
CP-42	6.0/N	64.0/N	512.0/N
CP-51	48.0/N	512.0/N	4096.0/N
CP-52	92.16/N	983.0/N	7864.0/N

*N = RPM

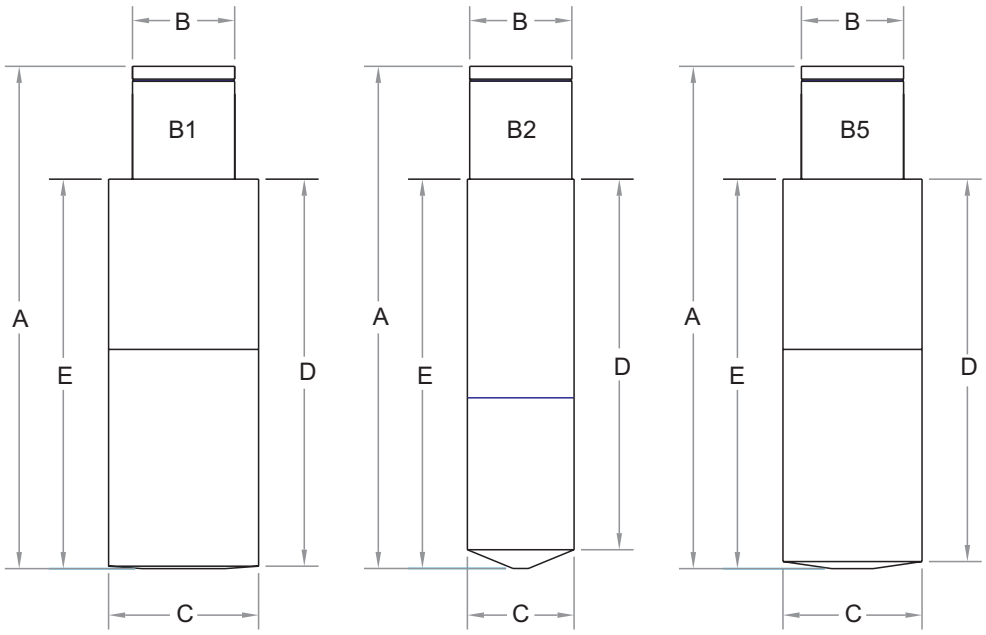
A.6 CAP Viscometer Spindle Dimensions and Shear Rates



Spindle No.	A	B-Diameter	C-Angle	D-Diameter	E	Shear Rate*
CAP-S-01	2.075 (52.71)	.187 (4.75)	0° -27'	1.190 (30.23)	.010 (0.25)	13.3N
CAP-S-02	2.075 (52.71)	.187 (4.75)	0° -27'	.945 (24.0)	.010 (0.25)	13.3N
CAP-S-03	2.075 (52.71)	.187 (4.75)	0° -27'	.750 (19.05)	.010 (0.25)	13.3N
CAP-S-04	2.075 (52.71)	.187 (4.75)	1° -48'	.945 (24.0)	.010 (0.25)	3.3N
CAP-S-05	2.075 (52.71)	.187 (4.75)	1° -48'	.750 (19.05)	.010 (0.25)	3.3N
CAP-S-06	2.075 (52.71)	.187 (4.75)	1° -48'	.553 (14.05)	.010 (0.25)	3.3N

***N = RPM**

A.7 PVS Rheometer Spindle Dimensions



Stator No.	A	B-Diameter	C-Diameter	D	E	Shear Rate*
B1	4.527 (114.99)	.925 (23.5)	1.358 (34.49)	3.507 (89.08)	3.527 (89.59)	1.703N
B2	4.524 (114.91)	.925 (23.5)	.967 (24.56)	3.354 (85.19)	3.524 (89.51)	.377N
B5	4.526(114.96)	.925 (23.5)	1.259 (31.98)	3.462 (87.93)	3.526 (89.56)	.85N

***N = RPM**

****Based on PVS-30 (HC) standard cup. Larger cups are available.**

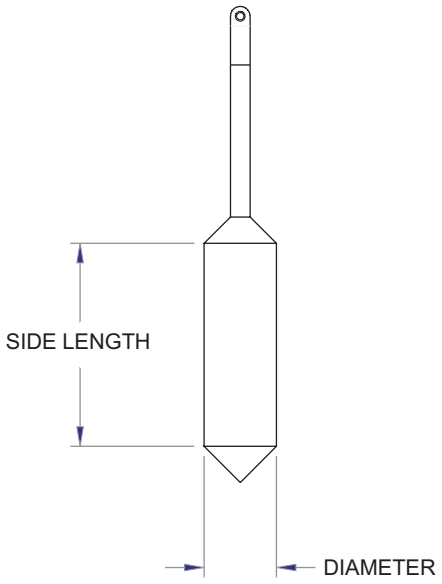
A.8 Thermosel System

SC4 Series Spindle Factors and Shear Rates

Spindle	Sample Size	LV	RV	HA	HB	Shear Rate (sec^{-1})
SC4-18	8.0	30/N*	320/N	640/N	2560/N	1.32N
SC4-21	8.0	46.88/N	500/N	1000/N	4000/N	0.93N
SC4-27	10.5	234.4/N	2500/N	5000/N	20M/N	0.34N
SC4-28	11.5	468.8/N	5000/N	10M/N	40M/N	0.28N
SC4-29	13.0	937.5N	10M/N	20M/N	80M/N	0.25N
SC4-31	10.0	300/N	3200/N	6400/N	25.6M/N	0.34N
SC4-34	9.5	600/N	6400/N	12.8M/N	51.2M/N	0.28N

*N = RPM M = 1000
The above values also apply to SC4-BS series spindles.

SC4 Series Spindle Dimensions



Spindle	Diameter	Side Length
SC4-18	0.688 (17.48)	1.249 (31.72)
SC4-21	0.660 (16.76)	1.230 (31.24)
SC4-27	0.463 (11.76)	1.300 (33.02)
SC4-28	0.370 (9.39)	1.260 (32.00)
SC4-29	0.300 (7.62)	1.070 (27.18)
SC4-31	0.463 (11.76)	0.990 (25.15)
SC4-34	0.370 (9.39)	0.954 (24.23)

Dimensions are in inches (mm). Dimensions also apply to SC4-BS spindles.

HT-2 Sample Chamber Dimensions

Diameter	Depth
0.750 (19.05)	2.550 (64.77)

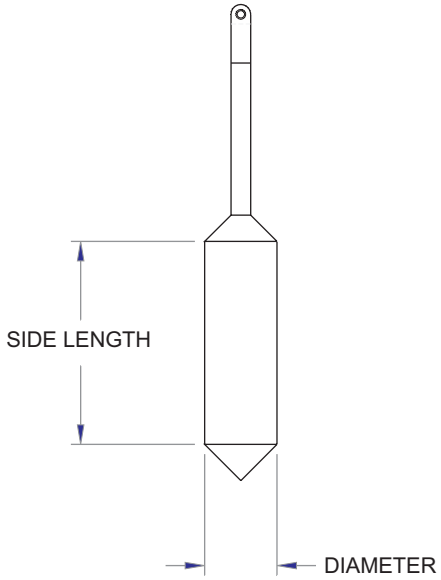
A.9 Small Sample Adapter

SC4 Series Spindle Factors and Shear Rates

Spindle/ Chamber	Sample Size (mL)	LV	RV	HA	HB	Shear Rate (sec^{-1})
SC4-14/6R	2.0	1172/N	12.5M/N*	25M/N	100M/N	0.40N
SC4-15/7R	3.0	468.8/N	5000/N	10M/N	40M/N	0.48N
SC4-16/8R	4.2	1200/N	12.8M/N	25.6M/N	102.4M/N	0.29N
SC4-18/13R	8.0	30/N	320/N	640/N	2560/N	1.32N
SC4-21/13R	8.0	46.88/N	500/N	1000/N	4000/N	0.93N
SC4-25/13R	16.0	4800/N	51.2M/N	102.4M/N	409.6M/N	0.22N
SC4-27/13R	11.0	234.4/N	2500/N	5000/N	20M/N	0.34N
SC4-28/13R	12.0	468.8/N	5000/N	10M/N	40M/N	0.28N
SC4-29/13R	13.0	937.5/N	10M/N	20M/N	80M/N	0.25N
SC4-31/13R	10.0	300/N	3200/N	6400/N	25.6M/N	0.34N
SC4-34/13R	10.0	600/N	6400/N	12.8M/N	51.2M/N	0.28N

*N = RPM M = 1000

SC4 Series Spindle Dimensions



Spindle	Diameter	Side Length
SC4-14	0.344 (8.74)	0.340 (8.64)
SC4-15	0.376 (9.55)	0.674 (17.12)
SC4-16	0.275 (6.99)	0.815 (20.70)
SC4-18	0.688 (17.48)	1.249 (31.72)
SC4-25	0.188 (4.78)	0.520 (13.21)
SC4-27	0.463 (11.76)	1,300 (33.02)
SC4-28	0.370 (9.39)	1.260 (32.00)
SC4-29	0.300 (7.62)	1.070 (27.18)
SC4-31	0.463 (11.76)	0.990 (25.15)
SC4-34	0.370 (9.39)	0.954 (24.23)

SC4 Series Sample Chamber Dimensions

Chamber	Diamenter	Depth
SC4-6R	0.500 (12.70)	1.110 (28.19)
SC4-7R	0.501 (12.73)	1.745 (44.32)
SC4-8R	0.515 (13.08)	1.584 (40.23)
SC4-13R	0.750 (19.05)	2.550 (64.77)

Dimensions are in inches (mm).

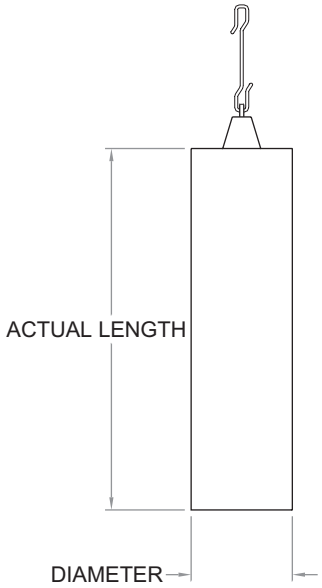
A.10 UL Adapter

UL Adapter Spindle Factors and Shear Rates

	LV	RV	HA	HB	Shear Rate (sec^{-1})
UL	6/N*	64/N	128/N	512/N	1.224N
DIN-UL	11.44/N	122.N	244/N	976/N	1.29N

*N = RPM Sample size 16.0 mL (end cap on).

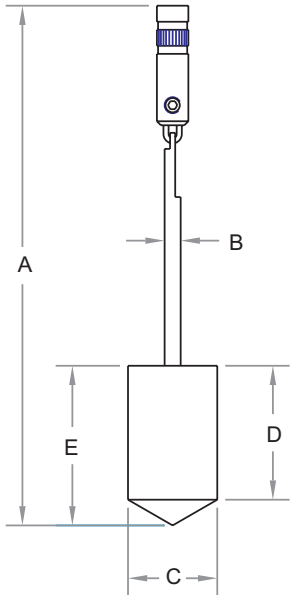
UL Adapter Dimensions



Spindle Effective Length*	Actual Length	Diameter	Chamber Inside Diameter
3.6366 (92.39)	3.5725 (90.74)	0.9902 (25.15)	1.0875 (27.62)

Dimensions are in inches (mm).
*Effective length includes correction for end effect and should be used in shear rate/shear stress equations. Actual length is given for reference only.

A.11 DIN Adapter Spindle Dimensions



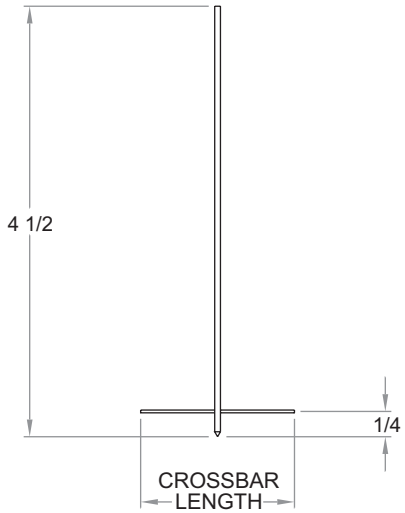
Spindle No.	A	B-Diameter	C-Diameter	D	E
HT-DIN-81	6.096 (175.42)	.125 3.18)	.6915 (17.56)	1.0373 (26.35)	1.237 (31.42)
SC4-DIN-82	5.219 (132.56)	.125 (3.18)	.6915 (17.56)	1.0373 (26.35)	1.237 (31.42)
SC4-DIN-83	4.526 (114.96)	.125 (3.18)	.4617 (11.73)	.6926 (17.59)	.826 (20.98)
ULA-DIN-85	6.066 (154.08)	.125 (3.18)	1.0026 (25.47)	1.504 (38.2)	1.793 (45.54)
ULA-DIN-86	3.911 (99.34)	.125 (3.18)	.6952 (17.66)	1.0428 (26.49)	1.244 (31.6)
ULA-DIN-87	3.500 (88.9)	.125 (3.18)	.4654 (11.82)	.6981 (17.73)	.833(21.16)

Spindle No.	Chamber No.	Chamber ID
HT-DIN-81	HT-2	.7500 (19.05)
SC4-DIN-82	SC4-13R	.7500 (19.05))
SC4-DIN-83	SC4-7R	.500 (12.7)
ULA-DIN-85	DAA-1	1.0875 (27.62)
ULA-DIN-86	ULA-DIN-6Y	.7540 (15.15)
ULA-DIN-87	ULA-DIN-6Y	.5048(12.82)

A.12 Helipath Stand

Travel Speed
7/8 inch (22.2 mm) per minute

T-Bar Spindle Factors



Spindle	LV	RV	HA	HB
T-A	187.5/N*	2000/N	4000/N	16M/N
T-B	374.4/N	4000/N	8000/N	32M/N
T-C	936/N	10M/N	20M/N	80M/N
T-D	1872/N	20M/N	40M/N	160M/N
T-E	4680/N	50M/N	100M/N	400M/N
T-F	9360/N	100M/N	200M/N	800M/N

*N = RPM
M = 1000 Maximum recommended speed: 10-12 RPM.

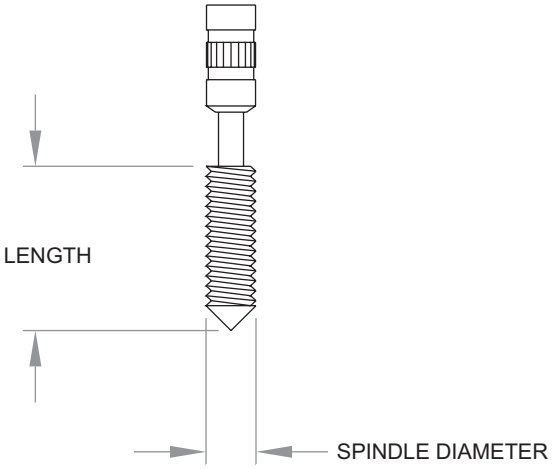
T-Bar Spindle Dimensions

Spindle	Crossbar Length
T-A	1.894 (48.1)
T-B	1.435 (36.4)
T-C	1.065 (27.1)
T-D	0.804 (20.4)
T-E	0.604 (15.3)
T-F	0.403 (10.9)

Dimensions are in inches (mm)

A.13 Spiral Adapter Dimensions

Spiral Spindle Dimensions

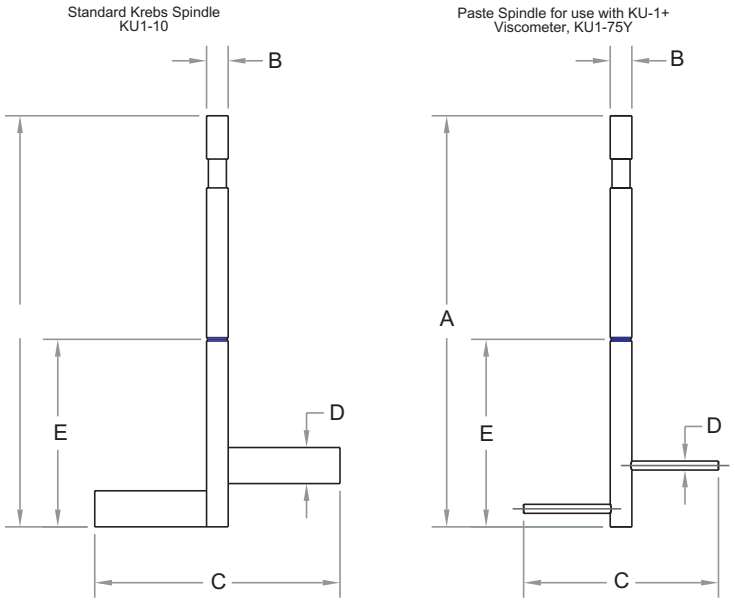


Spindle Diameter	Length
.250	.825

Spiral Chamber Dimensions

Diameter	Length
.275	.500

A.14 KU-1+ (Krebs) Viscometer Spindle Dimensions



Spindle No.	A	B-Diameter	C	D	E
KU1-10	3.562 (90.47)	.188 (4.77)	2.125 (53.98)	.312 (7.92)	1.625 (41.28)
KU1-75Y	3.562 (90.47)	.188 (4.77)	1.688 (42.88)	.078 (1.98)	1.625 (41.28)

APPENDIX B: ASTM Specifications

The following ASTM specifications describe the use of Brookfield Viscometers and accessories. Copies of these documents are available from Brookfield upon request.

C 965-81	Practices for Measuring Viscosity of Glass Above the Softening Point
C 1276-94	Standard Test Method for Measuring the Viscosity of Mold Powers Above their Melting Point Using a Rotational Viscometer
D 115-85	Methods of Testing Varnishes Used for Electrical Insulation
D 562-81	Standard Test Method for Consistency of Paints Using the Stormer Viscometer
D 789-91	Test Methods for Determination of Relative Viscosity, Melting Point, and Moisture Content of Polyamide (PA)
D 1076-88	Specification for Rubber-Concentrated, Ammonia Preserved, Creamed and Centrifuged Natural Latex
D 1084-88	Test Methods for Viscosity of Adhesives
D 1417-90	Methods of Testing Rubber Latices-Synthetic
D 1439-83a	Methods of Testing Sodium Carboxymethyl-cellulose
D 1824-90	Test Method for Apparent Viscosity of Plastisols and Organosols at Low Shear Rates by Brookfield Viscometer
D 2196-86	Test Methods for Rheological Properties on Non-Newtonian Materials by Rotational (Brookfield) Viscometer
D 2364-85	Standard Methods of Testing Hydroxyethyl-cellulose
D 2393-86	Test Method for Viscosity of Epoxy Resins and Related Components
D 2556-80	Test Method for Apparent Viscosity of Adhesives Having Shear Rate Dependent Flow Properties
D 2669-87	Test Method for Apparent Viscosity of Petroleum Waxes Compounded With Additives (Hot Melts)
D 2983-87	Test Method for Low-Temperature Viscosity of Automotive Fluid Lubricants Measured by the Brookfield Viscometer
D 2994-77	Methods of Testing Rubberized Tar
D 3232-88	Method for Measurement of Consistency of Lubricating Greases at High Temperatures
D 3236-88	Test Method for Apparent Viscosity of Hot Melt Adhesives and Coating Materials
D 3468-90	Standard Specification for Liquid-Applied Neoprene and Chlorosulfonated Polyethylene Used in Roofing and Waterproofing
D 3716-83	Method of Testing Emulsion Polymers for Use in Floor Polishes
D 3791-90	Standard Practice for Evaluating the Effects of Heat on Asphalts
D 4016-81	Test Method for Viscosity of Chemical Grouts by the Brookfield Viscometer (Laboratory Method)
D 4287-94	Standard Test Method for High-Shear Viscosity Using the ICI Cone/Plate Viscometer
D 4300-83	Test Method for Effect of Mold Contamination on Permanence of Adhesive Preparations and Adhesive Films
D 4402-87	Standard Method for Viscosity Determinations of Unfilled Asphalts Using the Brookfield Thermosel Apparatus
D 4889-93	Standard Test Methods for Polyurethane Raw Materials: Determination of Viscosity of Crude or Modified Isocyanates
D 5018-89	Standard Test Method for Shear Viscosity of Coal-Tar and Petroleum Pitches
D 5133-90	Standard Test Method for Low Temperature, Low Shear Rate, Viscosity/Temperature Dependence of Lubricating Oils Using a Temperature-Scanning Technique

APPENDIX C: References

References

The following publications are available from the publishers listed for further reading on the subject of rheology and viscosity measurement:

NON-NEWTONIAN FLOW AND HEAT TRANSFER
A.H.P. Skelland
John Wiley & Sons, New York, NY.

PAINT FLOW AND PIGMENT DISPERSION
Second Edition
Temple C. Patton
Interscience Publishers, New York, NY.

PRINCIPLES AND APPLICATIONS OF RHEOLOGY
Arnold G. Fredrickson
Prentice-Hall Inc., Englewood Cliffs, NJ.

RHEOLOGICAL METHODS IN FOOD PROCESS ENGINEERING
James F. Steffe
Freeman Press, E. Lansing, MI

RHEOLOGICAL PROPERTIES OF COSMETICS AND TOILETRIES
Dennis Laba
Marcel Dekker, Inc., New York, NY

VISCOMETRIC FLOWS OF NON-NEWTONIAN FLUIDS
Colemen/Markovitz/Noll
Springer-Verlag New York Inc., New York, NY.

VISCOSITY AND FLOW MEASUREMENT
Van Wazer/Lyons/Kim/Colwell
Interscience Publishers, New York, NY.

ISO standards may be purchased in the United States from:
American National Standards Institute
11 West 42nd Street, New York, NY. 10036
Phone: 212-642-4900; Fax: 212-302-1286

Outside the United States, please contact ISO's member in your country or:
International Organization for Standardization
1 rue de Varembe, 1211 Geneva 20, Switzerland

ASTM test methods are available from:
ASTM
1916 Race Street, Philadelphia, PA.
Phone: 215-299-5400; Fax: 215-977-9679

Brookfield Engineering Laboratories maintains a library of technical papers on viscosity measurement and control. Reprints are available upon request at no charge. A current listing of available papers and an order form are provided in the booklet, TECHNICAL PAPERS ON VISCOSITY MEASUREMENT AND CONTROL (DATA LIST 091-C).

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